

UNITED STATES OF AMERICA
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DEFENSE NUCLEAR FACILITIES SAFETY BOARD

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PUBLIC MEETING AND HEARING

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FRIDAY
OCTOBER 8, 2010

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The Board met in the Three Rivers
Convention Center, 7016 W. Grandridge
Boulevard, Kennewick, Washington, Peter S.
Winokur, Chairman, presiding.

PRESENT:

PETER S. WINOKUR, Chairman
JESSIE H. ROBERSON, Vice Chair
JOSEPH F. BADER, Board Member

LARRY W. BROWN, Board Member
JOHN E. MANSFIELD, Board Member

STAFF PRESENT:

TIMOTHY DWYER, Technical Director
RICHARD AZZARO, General Counsel

PANEL MEMBERS PRESENT:

GREG ASHLEY, BNI
DAVID BROCKMAN, DOE-ORP
DONNA BUSCHE, URS
STACY CHARBONEAU, DOE-ORP

DAVID DICKEY, Consultant
INES TRIAY, DOE-EM
DALE KNUTSON, DOE-ORP

PANEL MEMBERS PRESENT (Cont'd):

DAVID S. KOSSON, CRESP

LONI M. PEURRUNG, PNNL

FRANK RUSSO, BNI

PAUL RUTLAND, WRPS

LEO SAIN, URS

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P-R-O-C-E-E-D-I-N-G-S

8:00 a.m.

CHAIRMAN WINOKUR: Good morning.

My name is Peter Winokur. I am the Chairman of the Defense Nuclear Facilities Safety Board and I will preside over this public meeting and hearing.

At this time I would like to introduce my colleagues on the Safety Board. To my immediate left is Vice-Chairman Jessie Roberson and to her left is Mr. Larry Brown. On my right is Dr. John Mansfield and to his right is Mr. Joseph Bader. We five constitute the Board.

The Board's General Counsel, Richard Azzaro, is seated to my far left. The Board's Technical Director, Timothy Dwyer, is seated to my far right. Several members of our staff closely involved with oversight of the Department of Energy's defense nuclear facilities at Hanford are also present.

Today's meeting and hearing were

1 first publicly noticed in the Federal Register
2 on July 26, 2010, and renoticed for a change
3 of location on September 15, 2010. It is
4 being held open to the public in accordance
5 with the provisions of the Government in the
6 Sunshine Act.

7 The hearing is being broadcast
8 over the internet via video streaming; the
9 link can be found on the Board's website. A
10 video recording of the hearing will be made
11 available on the Board's website as soon as
12 possible after the hearing is concluded and
13 will remain available for at least 60 days.

14 A verbatim written transcript,
15 together with associated documents, will be
16 available for viewing and copying in the
17 Board's public reading room on the seventh
18 floor of the Board's headquarters in
19 Washington, D.C.

20 In accordance with the Board's
21 practice and as stated in the Federal Register
22 notice, we will welcome comments from

1 interested members of the public at the
2 conclusion of testimony for each of the three
3 sessions comprising this public meeting and
4 hearing.

5 A list of those speakers who have
6 contacted the Board is posted at the entrance
7 to this auditorium. We have listed the people
8 in the order in which they have contacted us
9 or, if possible, when they wish to speak. I
10 will call the speakers in this order and ask
11 that speakers state their name and title at
12 the beginning of their presentation.

13 There is also a table at the
14 entrance to this room with a sign-up sheet for
15 members of the public who wish to make a
16 presentation but did not have an opportunity
17 to sign up previous to this time. They will
18 follow those who have already registered with
19 us in the order in which they have signed up.

20 In order to give everyone wishing
21 to speak an equal opportunity, we ask
22 presenters to limit their statements to five

1 minutes. The Chair will then give
2 consideration to additional comments should
3 time permit.

4 Presentations should be limited to
5 comments, technical information, or data
6 concerning the subjects of this meeting and
7 hearing. The Board members may question
8 anyone making presentations to the extent
9 deemed appropriate.

10 The record of this proceeding will
11 remain open until November 7, 2010. The Board
12 reserves the right to further schedule and
13 regulate the course of this hearing, to
14 recess, reconvene, postpone, or adjourn this
15 meeting and hearing, and to otherwise exercise
16 its authority under the Atomic Energy Act of
17 1954, as amended.

18 Now let me proceed to explain the
19 Board's statutory authority for inquiring into
20 the matters that are the subject of this
21 public meeting and hearing. The Board's
22 enabling statute, now in effect for more than

1 twenty years, is found in the Atomic Energy
2 Act beginning in September 2286 of Title 42.

3 One section of this defines the
4 Board's role in the review of facility design
5 and construction. I quote, "The Board shall
6 review the design of a new Department of
7 Energy defense nuclear facility before
8 construction of such facility begins and shall
9 recommend to the Secretary, within a
10 reasonable time, such modifications of the
11 design as the Board considers necessary to
12 ensure adequate protection of public health
13 and safety.

14 During the construction of any
15 such facility, the Board shall periodically
16 review and monitor the construction and shall
17 submit to the Secretary, within a reasonable
18 time, such recommendations relating to the
19 construction of that facility as the Board
20 considers necessary to ensure adequate
21 protection of public health and safety.

22 An action of the Board, or a

1 failure to act, under this paragraph may not
2 delay or prevent the Secretary of Energy from
3 carrying out the construction of such a
4 facility."

5 The hearing begun yesterday
6 morning forms a part of the Board's continuing
7 effort to fulfill this statutory charge with
8 respect to the Waste Treatment and
9 Immobilization Plant, also known as the Waste
10 Treatment Plant. The record of the hearing,
11 both oral and written, will be used by the
12 Board to formulate recommendations to the
13 Secretary of Energy for this critical project.

14 These recommendations may take the
15 form of a formal Recommendation to the
16 Secretary or may be transmitted to the
17 Department through letters or informal
18 exchanges between technical counterparts. The
19 Board's oversight responsibilities continue
20 through completion of construction, testing,
21 operation, and eventual decommissioning of
22 these facilities.

1 The Board's statutory charter is,
2 like that given to other agencies operating
3 under the Atomic Energy Act, the protection of
4 the public health and safety, including safety
5 of the workers.

6 In the case of the Waste Treatment
7 Plant, however, this statutory charge is made
8 more complex because proper construction and
9 operation of the plant is critical in
10 resolving the underlying health and safety
11 problem, mainly the large volume of toxic and
12 radioactive wastes now stored in underground
13 tanks at Hanford.

14 Many of these tanks are already 67
15 years old, and would be almost 100 years old
16 by the end of the projected treatment mission.
17 Consequently, it is not enough, in this case,
18 for the Board to focus solely on whether the
19 construction of the Waste Treatment Plant will
20 not suffer accidents harmful to workers or the
21 public -- it must operate safely and
22 effectively for many decades to remediate the

1 safety hazard represented by tank waste.

2 The Board has, therefore, inquired
3 into many issues that involve a mixture of
4 accident risk and successful and efficient
5 long-term operations.

6 At this time, I'd like to provide
7 some additional background on the history of
8 this project. The Hanford high-level waste
9 tanks began receiving waste in the 1940s. As
10 the initial single shell tanks were being
11 constructed, they were designed for about a
12 20-year life.

13 Over the seven decades of
14 operation of the tank farms, poor chemical and
15 configuration control of the wastes has
16 created a much more challenging problem for
17 understanding the chemistry and properties of
18 the waste, as well as getting them mobilized,
19 than exists at other sites such as the
20 Savannah River Site and the Idaho Cleanup
21 Project.

22 Characterization of this waste

1 remains problematic. The first time that a
2 single shell tank was suspected of leaking was
3 in the mid-1950s. Many single-shell tanks
4 have been proven leakers since then. The
5 leakage exacerbates the need to get these
6 wastes out of the tanks and in a stable form
7 suitable for eventual disposal.

8 The Department of Energy's
9 solution to removing and stabilizing the waste
10 to reduce the current and future threats to
11 health and safety is the Waste Treatment
12 Plant.

13 The Waste Treatment Plant Project
14 was initiated in the mid-1990s. This is a
15 first of a kind project. The Board's formal
16 oversight of the project began in earnest
17 after a privatization effort was abandoned in
18 2002. The Board has been advising the
19 Department about our concerns related to the
20 design basis safety requirements and their
21 potential impact on operational safety
22 throughout the life of the project.

1 Since initiating the project, the
2 Department has pursued internal and external
3 reviews of the project, obtaining advice from
4 experts in academia, the chemical and process
5 industries, and its national laboratories to
6 help inform the design, safe operation and
7 performance of the plant over its projected
8 40-year operational life.

9 It is important to note that the
10 Department undertook a significant redesign
11 effort starting in 2009, even though the
12 design of the plant was more than 70 percent
13 complete. The redesign of the plant is now
14 over 80 percent complete and construction of
15 its pre-treatment facility is more than 30
16 percent complete.

17 Recently, the Department indicated
18 to the Board that it is transitioning the
19 Waste Treatment Plant project from a design
20 and construction project to one of
21 construction and commissioning. The
22 Department has referred to this transition as

1 "pivoting."

2 As such, the Department is
3 planning to wrap up its design actions by
4 establishing the final design criteria for the
5 plant's structures, systems, and components.
6 The pivot is intended to provide a defined
7 path forward to finish the design of the
8 systems and components that have not been
9 finalized and to resolve any outstanding
10 technical issues.

11 The Board is deeply concerned that
12 the plant may be commissioned before several
13 key technical issues are fully resolved. Once
14 operational and exposed to radioactive waste,
15 options for design changes in black and hot
16 cells will be extremely limited, costly, and
17 expose workers to hazardous situations. To
18 the maximum extent possible, solutions must be
19 accommodated before commissioning. A learn-
20 as-we-go philosophy does not seem prudent for
21 this facility.

22 Given that the project is now

1 pivoting, wrapping up design and focusing on
2 commissioning, it is a crucial time to have
3 DOE [Department of Energy] explain where they
4 are, where they are going, what remains to be
5 done, and in what time frame. Also, implicit
6 in the Board's statutory mandate is keeping
7 the public appropriately informed of issues
8 affecting public health and safety. Those are
9 the goals for these proceedings.

10 The proceedings began last month
11 when DOE provided over two hundred pages of
12 written answers to Board questions. These
13 questions and answers are available on the
14 Board's website and will become a part of the
15 record of these proceedings. I want to take a
16 moment to thank the Department for its timely
17 response to these questions.

18 We began yesterday to explore some
19 of these answers to gain a more complete
20 understanding. However, because of the large
21 volume of information that must be discussed,
22 a lack of further inquiry in this hearing or

1 in the near future should not necessarily be
2 viewed as satisfaction on the part of the
3 Board with either a previous written or verbal
4 answer.

5 The Board noted in its transmittal
6 of questions to DOE in August, 2010 that these
7 questions should be viewed as a starting point
8 for the discussions that will occur during
9 this public meeting and hearing.

10 There are several areas of the
11 Waste Treatment Plant design in which the
12 Board has concerns with the safety and
13 ultimate operation for the decades the plant
14 must operate. These areas include:

15 The ability of the plant to
16 adequately mix the wastes after they are
17 transferred from the tank farms into the
18 plant.

19 The hydrogen control strategy for
20 dealing with the hydrogen gas that is
21 inevitably generated by the high-level wastes.

22 The implementation of safety

1 controls necessary to implement the hydrogen
2 control strategy.

3 The likelihood that limitations on
4 the plant's operating envelope resulting from
5 the performance of the plant's mixing systems
6 will result in more demands on the tank farms
7 to deliver waste that meets restrictive waste
8 acceptance criteria or the need to provide
9 alternative processing capability.

10 The third session of the Board's
11 hearings -- this morning's session -- is going
12 to concentrate on concerns with particular
13 aspects of the revised safety design strategy.
14 We are trying to understand the ability of the
15 plant to safely, effectively, and efficiently
16 process waste delivered from the tank farms so
17 that it can be vitrified for eventual
18 disposal.

19 This involves the treatment of
20 waste that, by its very nature, generates a
21 significant quantity of hydrogen gas.

22 Hydrogen gas can, under the right

1 circumstances, accumulate in process piping
2 and become an explosion hazard, with the
3 potential to seriously damage process piping.

4 In extreme cases, such explosions
5 could breach the primary confinement boundary,
6 resulting in a potential hazard to workers or
7 even the public, and the potential
8 interruption of waste processing for long
9 periods. DOE has developed a hydrogen-in-
10 pipes-and-ancillary-vessels, HPAV [hydrogen-
11 in-pipes-and-ancillary-vessels], safety design
12 that is intended to contain the effects of a
13 hydrogen explosion in the piping system or, in
14 extreme cases, actively prevent the hydrogen
15 explosion. The design approach is new and, as
16 of today, incomplete.

17 We have requested that the
18 Department's expert in hydrogen explosions
19 from academia participate in today's panel
20 discussion. We had also invited the Team
21 Leader from the HPAV Independent Review Team
22 but he was not able to be with us today.

1 We have also asked for
2 participation from project design personnel
3 from Bechtel National, Incorporated, URS
4 Corporation, as well as the Department's
5 responsible personnel for managing the
6 project.

7 That concludes my opening remarks.
8 I will now ask my fellow Board members if they
9 have opening remarks before we begin the
10 testimony.

11 Hearing no such request, I would
12 like to invite the Assistant Secretary of
13 Energy for Environmental Management, the
14 Honorable Ines Triay, to make some opening
15 remarks.

16 DR. TRIAY: I appreciate the
17 opportunity to be here these last two days to
18 discuss our initiatives in assuring that we
19 will define, construct, and commission the
20 Waste Treatment and Immobilization Plant, WTP
21 [Waste Treatment and Immobilization Plant], so
22 that it can operate safely and reliably.

1 I would also like to introduce
2 some of the senior safety leadership from the
3 Department of Energy who have traveled to
4 Washington State to support these discussions.
5 Dr. Steve Krahn, to my right, is the Deputy
6 Assistant Secretary for Safety and Security in
7 the Office of Environmental Management.

8 Mr. Richard Lagdon, to my left, is
9 the Chief of Nuclear Safety for the Department
10 of Energy. The three of us represent 100
11 years of nuclear safety experience. Along
12 with all of our work colleagues at the Waste
13 Treatment Project we represent many hundreds
14 of years of experience of technically complex
15 and high-risk projects such as the Waste
16 Treatment Plant and tank farms.

17 As owner and operator of multiple
18 projects through the Department's complex
19 overall our nuclear safety record has been
20 exemplary. Our commitment to a safe,
21 efficient, and effective Waste Treatment Plant
22 is embodied by the three of us and our work

1 colleagues in the Department.

2 Safe operations including safety
3 of the public, safety of our workers, and
4 protection of the environment are paramount to
5 the Office of Environmental Management and
6 have been the cornerstone of my career.

7 With respect to the Waste
8 Treatment Plant you have heard the Deputy
9 Secretary's and the Federal Project Director's
10 experience and perspectives on the importance
11 of this facility to fulfilling the
12 Department's mission to safely treat the
13 Hanford tank waste.

14 I also devote a great deal of my
15 efforts to the Waste Treatment Plant and the
16 Tank Waste Program. We have over 15 years of
17 experience treating tank waste at the Savannah
18 River site which contains twice the total
19 radiation source than the Hanford tank farms.

20 High-level waste produces hydrogen
21 which can be flammable or detonable in
22 sufficient quantities so the Waste Treatment

1 Plant will be protected with active safety
2 systems to ensure hazardous concentrations of
3 gases don't accumulate.

4 Conditions can exist in the piping
5 and inline components where the waste may
6 remain stagnate. If a sufficient
7 concentration of hydrogen were to accumulate
8 and mixed with an oxidant and if an ignition
9 source were present, the gas mixtures could
10 ignite creating the postulated hydrogen event.

11 The piping in vessels that contain
12 high-level waste, primarily in the pre-
13 treatment and high-level waste facilities, are
14 the primary boundaries for this waste. The
15 Waste Treatment Plant contractor has developed
16 the design criteria for the piping to prevent
17 failures from perforations and detonations.
18 The Department has reviewed and approved those
19 criteria.

20 The project's design has always
21 included elements of both active safety
22 controls to prevent an HPAV event from

1 occurring and passive safety features to
2 assure piping integrity should an HPAV event
3 occur with the ultimate goal of ensuring that
4 the piping and inline component primary
5 confinement boundaries are not breached by a
6 postulated hydrogen event.

7 In April of 2006 the Department
8 issued a Safety Evaluation Report that
9 addressed criteria for HPAV events. In that
10 safety evaluation report DOE approved a
11 strategy that relied primarily on active
12 controls to prevent HPAV events. However, the
13 Safety Evaluation Report also included
14 provisions for passive controls for piping.

15 At that time the BNI [Bechtel
16 National Incorporated] had assessed that pipe
17 sizes less than or equal to two inches in
18 diameter could meet the passive design. The
19 Safety Evaluation Report further stated that
20 limited plastic behavior would be approved
21 when qualified by a supporting risk assessment
22 that should include a best estimate for the

1 facility incorporating estimation of
2 probability, location, and intensity of
3 hydrogen events.

4 Interactions with the Board and
5 staff at that time indicated agreement with
6 this approach. In response to ongoing
7 evaluation of hydrogen events, BNI began a
8 testing program to evaluate the consequences
9 of HPAV events on piping and complex component
10 designs such as PUREX [Plutonium Uranium
11 Extraction] connectors.

12 In 2009 the manager of the Office
13 of River Protection initiated several
14 independent reviews to determine whether the
15 2006 HPAV strategy both concerns from an
16 operability standpoint and whether an
17 alternative strategy could now be supported.
18 As a result of the recommendations from those
19 reviews, the Department directed the
20 contractor to propose an HPAV strategy that is
21 less dependent on active controls.

22 The Department directive for a

1 design with fewer HPAV active controls did not
2 constitute a significant redesign effort as
3 was mentioned in the opening remarks by the
4 Board. In fact, the HPAV controls have always
5 been an additive layer of controls that do not
6 change the innate waste process design
7 functions but add additional controls that
8 could disrupt efficient operations and
9 increase operational risk to plant
10 availability and worker safety.

11 The contractor has recommended an
12 approach that continues to rely on active and
13 passive features but with a reduced number of
14 active controls. The result in superior
15 design will reduce exposure to workers,
16 improve operational efficiency, thereby
17 facilitating more expeditious completion of
18 the tank waste mission and reduce risk of
19 facility or system contamination.

20 The specifics of the design
21 approach to protect against a postulated
22 hydrogen events rely on passive engineer pipe

1 component pressure boundary for piping up to
2 four inch in diameter where it can be shown
3 that the resulting loads on the piping and in
4 like components meet the approved design
5 criteria. Active controls where the
6 postulated hydrogen events could cause the
7 loads on piping and inline components to
8 exceed acceptance criteria.

9 The design of piping systems in
10 the Waste Treatment Plant ensures that an HPAV
11 event in the piping will not adversely affect
12 the ability of the piping on inline components
13 to perform their intended safety function,
14 will not render the piping inoperable, will
15 not introduce additional hazardous risks to
16 workers or have significant adverse impact on
17 WTP operations thereby facilitating efficient
18 plant operations.

19 In advancing the latest industry
20 experience with risk analysis the project also
21 completed evaluation of rigorous test programs
22 and developed the HPAV quantitative risk

1 analysis tool to organize application of the
2 experimental results to specific pipe routes
3 as required for ASME Code compliance [American
4 Society of Mechanical Engineers]. The HPAV
5 testing was conducted at the California
6 Institute of Technology by Dr. Shepherd who is
7 on the panel, and at Southwest Research
8 Institute in San Antonio, Texas.

9 From these test programs the
10 project has improved its understanding of HPAV
11 phenomena which include improved understanding
12 of gas phenomenology, validation that the
13 stainless steel piping is robust relative to
14 HPAV events, and that the piping shows minimal
15 or no permanent deformation following repeated
16 detonations, greater insight into the response
17 of piping to high frequency oscillations,
18 important design information regarding
19 components, test data available to benchmark
20 analytical models.

21 The QRA [Quantitative Risk
22 Analysis] provides an extremely insightful

1 tool from a safety perspective. The QRA
2 employs a multi-functional team of design,
3 operations, and safety personnel to analyze
4 the potential for hydrogen events by reviewing
5 the details of each path affected route and
6 the number of times that route is expected to
7 be used over the life of the plant, the normal
8 and not normal operating conditions for each
9 HPAV affected system using the structure
10 analysis of the event fault tree.

11 The event and fault tree logic
12 facilitates the review and response by looking
13 at loss of power, component failures, operator
14 errors, and other conditions that allow waste
15 to remain stagnate for extended periods. This
16 approach has been reviewed by the HPAV
17 Independent Review Team which consisted of 12
18 independent experts with a combined industry
19 experience of 450 years spanning the range of
20 technical disciplines applicable to the HPAV
21 strategy.

22 While Dr. Mattson is not able to

1 be here today to testify on the team's efforts
2 due to a death in his immediate family, I will
3 summarize the team's review. The HPAV
4 Independent Review Team concluded that
5 following implementation of the team's finding
6 there is high confidence that the QRA approach
7 is acceptable for the loads to be used in
8 design and that there is low probability of
9 exceeding either their frequency or their
10 magnitude.

11 The best estimate of pipe stresses
12 and strains computed from the defined loads in
13 the manner proposed by BNI are not likely to
14 be significantly exceeded. The combination of
15 QRA load definitions, best estimate piping
16 system response calculations, and conservative
17 acceptance criteria developed pursuant to the
18 piping code B31.3 provides a reasonable
19 balance of probabilistic and deterministic
20 elements appropriate for design of HPAV piping
21 and components.

22 The net result of this approach to

1 design will be a low probability of pipe
2 failure if hydrogen explosions occur. I
3 considered this industry endorsement evidence
4 that the Department has ensured that safety
5 and quality of the WTP design for HPAV events.

6 We met with you on August 24th and
7 September 24th to review the project's
8 implementation plan for solving the
9 Independent Review Team findings and
10 recommendations. I endorse the project's plan
11 and we are committed to continuing
12 interactions with the Board and its staff as
13 we implement the findings and recommendations
14 and complete the designs.

15 We will ensure the inputs and
16 assumptions of the QRA are adequately
17 protected for the operational life of the
18 facility. Finally, we will incorporate
19 insights from the QRA application into our
20 response to the Defense Nuclear Facility
21 Safety Board Recommendation 2009-1 which
22 pertains to the need for standards governing

1 risk applications.

2 In closing, I would like to state
3 that the evolution of the HPAV analysis and
4 design criteria is part of the normal DOE
5 process that may establish very conservative
6 approaches in the early stages of design but
7 changes to allow improvements to the plant's
8 design and operation as design evolves and
9 assessing to understand hazards is completed.

10 These efforts do not result in a
11 significant redesign of the Waste Treatment
12 Plant systems but improved design and
13 operational efficiency and reduce risk in
14 support of the WTP mission to process waste.

15 Finally, no design changes have
16 been implemented using the HPAV analysis and
17 design criteria and none will be made until
18 the finding resolutions are reviewed by the
19 Independent Review Team and are closed.

20 I would like to give the floor to
21 Mr. Richard Lagdon who will address the last
22 issue that we were discussing yesterday.

1 MR. LAGDON: Chairman Winokur,
2 Members of the Board, and staff, I appreciate
3 the opportunity to present for the record my
4 statement regarding the use of deposition
5 velocity at the Waste Treatment Plant. I
6 would also like to thank Dr. Triay for
7 recognizing my role in addressing this issue.

8 My position as the Chief of
9 Nuclear Safety was created in response to
10 Defense Nuclear Facility Safety Board
11 Recommendation 2004-1. One of my
12 responsibilities is to ensure safety is being
13 appropriately addressed by the line. I take
14 this responsibility very seriously.

15 MAX-2 Code Guidance was developed
16 and accepted by the Defense Nuclear Facility
17 Safety Board in 2004 as part of the
18 Department's effort to improve the software
19 quality assurance of software utilized in
20 safety-related applications.

21 This guidance specified generic
22 conservative values for use across the

1 complex. These values were based on NRC
2 [Nuclear Regulatory Commission] requirements
3 with similar applicability for facilities
4 operated by DOE.

5 When evaluating the conditions
6 specific for the Waste Treatment Plant I
7 reevaluated the technical basis contained in
8 NRC regulations and standards. This
9 evaluation was published in September 2009.

10 Because the evaluation continued
11 to be challenged because of its use of 1
12 centimeter per second for deposition velocity,
13 I solicited the independent technical review
14 of a nationally recognized expert, Dr. John
15 Tell, on the subject of atmospheric dispersion
16 and modeling to review the issues and provide
17 recommendations to the Department.

18 The question to be evaluated is
19 the MAX-2 code as implemented based on
20 documentation assuming 1 centimeter per second
21 deposition velocity for particles sufficiently
22 conservative for the Hanford site such that

1 the target dose to the public is not
2 underestimated at the 95 percentile level.

3 Dr. Tell concluded that the MAX-2
4 results and the analysis of the Waste
5 Treatment Plant are conservative and meet the
6 objectives of the assessment question.

7 CHAIRMAN WINOKUR: Excuse me, Mr.
8 Lagdon. We are going to need to finish up
9 your testimony here in the next couple of
10 minutes.

11 MR. LAGDON: Yes, sir.

12 CHAIRMAN WINOKUR: I don't know if
13 you have a lot to go.

14 MR. LAGDON: No, I've got one more
15 paragraph, sir.

16 CHAIRMAN WINOKUR: Wonderful.
17 Thank you.

18 MR. LAGDON: Okay. In reviewing
19 the revised severity level calculations the
20 impact on the analysis will not affect the
21 design of WTP because of the small difference
22 in the impacts using a more conservative

1 number.

2 I will review this analysis with
3 the Waste Treatment Plant safety analysis
4 personnel in the near future and issue a
5 revised technical paper reflecting the
6 recommendations of an independent expert
7 review. This will ensure that the Waste
8 Treatment Plant is designed to the appropriate
9 criteria and a conservative analysis exist
10 such that the target dose to the public is not
11 underestimated at the 95th percentile level.

12 DR. TRIAY: Chairman Winokur, Dr.
13 Krahn will be submitting for the record our
14 steps as the head of the Technical Authority
15 Board to ensure compliance of the QRA process
16 with 10 CFR 830 [Code of Federal Regulations].

17 CHAIRMAN WINOKUR: Thank you. I
18 appreciate it. Thank you, Dr. Triay. Thank
19 you Mr. Lagdon and Dr. Krahn.

20 The session will continue with
21 testimony offered by members of the Board
22 staff. I ask each staff member who offers

1 testimony to begin by stating his name and
2 position for the record.

3 MR. KASDORF: Good morning, Mr.
4 Chairman, members of the Board. My name is
5 Roy Kasdorf. With me are Mr. Steven Stokes
6 and Mr. Scott Suffridge, staff leads for the
7 Hydrogen Control and WTP. I am the lead for
8 the Board's Nuclear Facility, Design, and
9 Infrastructure group.

10 I am responsible for ensuring that
11 the staff reviews of the design and
12 construction of the Waste Treatment and
13 Immobilization Plant are completed consistent
14 with the Board's mission.

15 In this morning's meeting the
16 Board is considering safety-related aspects of
17 the pretreatment design and operations,
18 specifically the safety design strategy for
19 control of hydrogen. I will discuss the
20 hazards presented by the hydrogen process
21 vessels, piping and inline components and the
22 Department of Energy's revised safety strategy

1 to control this hazard.

2 As I've said in previous sessions,
3 over the past eight years the Board's staff
4 has been reviewing the pretreatment facility
5 design and safety basis development. The
6 staff recognizes that operation of the WTP is
7 vital to the remediation of the Hanford site.

8 The WTP is the primary means for
9 reducing the risk resulting from storage of
10 high-level waste in Hanford's tanks. As such,
11 the staff recognizes that the WTP must operate
12 efficiently and safely over the entire
13 duration of the multi-decade mission.

14 The staff concerns are
15 fundamentally related to safety issues but
16 many of the safety issues would also result in
17 significant operational problems such as the
18 build up of material in vessels, plugging or
19 bursting pipes. Such operational problems
20 would delay processing of Hanford tank waste.
21 The Board believes that such a delay is a
22 safety concern.

1 A little bit of background.

2 Hydrogen gas is produced in all waste tanks
3 depending on the amount of radiation present,
4 hydrogen containing chemicals present, and the
5 concentration of hydrogen scavengers. There
6 are three distinct mechanisms that produce
7 hydrogen gas from the tank waste; radiolysis,
8 which is radiation interacting with molecules
9 containing hydrogen breaking the chemical
10 bonds to produce hydrogen gas. Radiolysis
11 typically generates the largest amounts of
12 hydrogen gas in WTP.

13 Thermolysis, which is the
14 deformation of organic molecules containing
15 hydrogen in the presence of radiation produces
16 hydrogen gas. Due to the relatively low
17 temperatures in WTP thermolysis is not a large
18 contributor to the overall gas generation in
19 WTP.

20 The third mechanism is corrosion
21 of metal piping in vessels generates hydrogen
22 but this will be insignificant in WTP due to

1 the corrosion resistant materials used to make
2 up the piping in vessels. In order for
3 hydrogen gas to become an explosion hazard two
4 other factors must also be present with the
5 hydrogen; a source of oxygen and an ignition
6 source.

7 There are two potential sources of
8 gaseous oxygen in the Hanford's waste. First,
9 oxygen can become entrained in the waste, for
10 example from sparge that are used to mix some
11 vessels. Second, oxygen can be present in the
12 form of nitrous oxide, a gas produced in the
13 waste from compounds containing nitrogen.

14 There are several potential
15 ignition sourcing including mechanical
16 components and compressive heating of the gas
17 itself. Unfortunately, hydrogen gas has one
18 of the lowest minimum ignition energies known
19 which is why the control of ignition sources
20 is rarely, if ever, relied upon as a control
21 strategy for preventing hydrogen explosions.

22 DOE began the hydrogen design

1 effort in response to two explosion events at
2 nuclear power stations in 2001, one in Japan,
3 the other in Germany. DOE correctly
4 recognized that there were some more potential
5 explosion hazards associated with hydrogen and
6 piping systems in WTP.

7 DOE's initial hydrogen control
8 strategy was conservative and focused on
9 preventing hydrogen explosions in vessels and
10 explosions with the potential to deform
11 piping. Ultimately DOE and BNI developed what
12 the Board considered to be a conservative
13 hydrogen and pipe safety design strategy.

14 In the Board's quarterly report to
15 Congress dated October 17, 2007, the Board
16 made the following observation: DOE has
17 developed a conservative design criterion.
18 The Board believes the design criterion is
19 adequate for its intended purpose and the
20 issue is considered resolved.

21 However, in early 2009 DOE formed
22 a hydrogen and piping in ancillary vessels, an

1 HPAV, assessment team to evaluate the controls
2 and design approach for the control of
3 hydrogen in WTP. As discussed in previous
4 sessions, this action was taken due to DOE's
5 concern with complexity in the WTP.

6 On February 26, 2009 this team
7 provided DOE with several recommendations that
8 deviated significantly from the hydrogen
9 control strategy considered acceptable by the
10 Board in 2007. These recommendations are the
11 basis for DOE's revised hydrogen and pipe
12 safety design strategy.

13 The team's recommendations can be
14 summarized as follows. First, DOE should
15 reevaluate select assumptions and methods used
16 in accident analysis. Second, DOE should
17 separate the evaluation approach for the
18 safety case and the mission case. The team
19 judged that hydrogen explosions was primarily
20 a mission case concerned with operational
21 availability and that the safety concern was
22 mitigated by the building and its confinement

1 ventilation system.

2 Third, DOE should adopt a mission
3 risk-based approach to evaluate the physical
4 phenomena and potential consequences of
5 hydrogen accumulation. Lastly, DOE should
6 reduce the levels of conservatism in the
7 evaluation methodology and structural
8 acceptance criteria.

9 Subsequently, in its quarterly
10 report to Congress dated June 22, 2009 the
11 Board observed that there are several of these
12 recommendations were inadequately supported.
13 The prime example was the creation of a
14 mission case to justify allowing hydrogen
15 explosions that could result in breaching the
16 primary confinement boundary. The Board
17 emphasized that implementation of the
18 recommendations would be detrimental to the
19 safety of the facility.

20 Since then DOE has decided to
21 pursue some but not all of the team's
22 recommendations. DOE approved a revised

1 design criteria on February 15th of this year
2 that allowed hot cell piping to undergo
3 permanent deformation, its bulge, due to an
4 explosion but did not accept the primary
5 boundary could rupture and did not allow
6 permanent deformation of piping in the black
7 cells.

8 The approved approach uses risk-
9 based quantitative risk analysis, QRA, to
10 calculate the frequency and severity of
11 hydrogen explosions in each run of piping and
12 then applies those predictions to design the
13 piping and select the safety controls.

14 The staff believes that DOE's
15 revised approach is more complex, less
16 conservative, and reduces the margin of safety
17 for the hot cell piping design compared to the
18 original design approach adopted in 2007.

19 In its April 15, 2010 quarterly
20 report to Congress the Board made the
21 following observation. The Board is concerned
22 that the design criteria lacks sufficient

1 specificity to ensure that the design will
2 maintain the integrity of the primary
3 confinement boundary as intended by DOE Order
4 420.1, Facility Safety.

5 The primary issues were DOE
6 invoked a provision in the code that permits
7 the facility owner to approve alternative
8 methods for piping system design. Although
9 this latitude exists, the alternative methods
10 must be consistent with DOE's directives for
11 the design of defense nuclear facilities such
12 as DOE Order 420.1.

13 The proposed strategy uses QRA to
14 determine the peak pressure and the frequency
15 of explosions. DOE has no standard governing
16 the application of QRAs. BNI intends to test
17 inline components, valves, and pumps that did
18 not specify the specific methods or the
19 criteria for the qualification.

20 DOE's justification for allowing
21 permanent deformation is that operators can
22 inspect the hot cell piping, observe leaks,

1 and repair failed components. However, the
2 facility design does not include the
3 capability to readily detect an explosion.
4 Further, repair or replacement of the piping
5 could be time consuming, cause significant
6 disruption of plant operations, and
7 potentially result in considerable risk to
8 workers performing the work.

9 In April 2010 BNI chartered the
10 Hydrogen Pipes and Ancillary Vessels
11 Independent Review Team, the HIRT. The HIRT's
12 review was intended to provide added assurance
13 that the criteria and the methodology used to
14 design WTP to withstand the affects of
15 postulated hydrogen explosions was technically
16 defensible and conservative to ensure the
17 safety and reliability of the WTP design.

18 At the time the HIRT conducted its
19 review BNI had not completed the final design
20 approach, the approach for qualifying inline
21 components, or the QRA. Further, several key
22 input documents reviewed by the HIRT were

1 still in draft form.

2 On April 12, 2010 the HIRT issued
3 its final report which identified 35 findings
4 and 32 recommendations. The HIRT concluded
5 that the design approach for hydrogen and
6 piping components was acceptable provided BNI
7 resolve the findings before implementing the
8 revised approach.

9 The HIRT provided the
10 recommendations as discretionary improvements
11 that DOE and BNI should consider for making
12 long-term improvements when using risk-formed
13 approach design. DOE approved a closure plan
14 to address both the findings and
15 recommendations from the HIRT report on
16 September 16, 2010.

17 The closure plan describes BNI's
18 response to resolve each of the HIRT's
19 findings, the process to be used to document
20 the actions taken to respond to each finding,
21 and the process to be used to communicate
22 BNI's actions to the HIRT team for review and

1 eventual closing of the findings.

2 The closure plan also identified
3 which recommendations will be implemented by
4 BNI and which will not. DOE and BNI have
5 still not completed the final design method to
6 implement the revised safety design strategy
7 for HPAV. Further, several elements of the
8 revised HPAV safety design strategy have never
9 been completed.

10 I'm going to repeat that because
11 it goes to the heart of the staff's concerns.
12 There are several elements of the safety
13 strategy that have never been completed and
14 those are the methodology for the QRA, the
15 requirements for qualification of inline
16 components, and the final set of calculations
17 supporting the design criteria.

18 BNI is still working to resolve
19 findings from the HIRT and several of the
20 findings are significant. The staff cannot
21 complete its reviews of the HPAV safety design
22 strategy until the methodology and the overall

1 approach have been completed and examples of
2 its use have been demonstrated.

3 There are three key aspects of the
4 strategy that must be completed or resolved.
5 Those are the QRA, development of the safety
6 basis to implement the strategy and the
7 resolution of the HIRT findings.

8 The staff is concerned that DOE's
9 use of QRA, which is the most important aspect
10 of the revised hydrogen in pipes strategy that
11 remains to be completed. It is also the most
12 novel element of the revised strategy in that
13 DOE has never before attempted to use a
14 probabalistic design tool like the QRA to
15 design the primary confinement boundary for a
16 nuclear facility.

17 BNI is using the QRA to predict
18 both frequency and peak pressure of the range
19 of potential hydrogen explosions in the WTP
20 piping. This information is used to develop
21 process piping response that is then compared
22 to BNI's design criteria to determine if the

1 piping can withstand the explosion.

2 For those cases in which the pipe
3 is predicted to deform beyond the allowed
4 criteria, the piping system is redesigned or
5 an active control is determined to be
6 necessary.

7 There are several noteworthy
8 concerns regarding the use of QRA for the WTP.
9 First, and I am repeating this, there are no
10 DOE requirements to govern the use of QRA to
11 ensure it is properly incorporated into the
12 nuclear safety basis. Second, DOE's current
13 safety-related orders and standards typically
14 require the use of a deterministic approach to
15 develop the nuclear safety basis.

16 Lastly, the assumptions used to
17 develop the QRA fault trees and establish
18 event frequencies and severities become part
19 of the safety basis. These assumptions must,
20 therefore, be protected in the same fashion as
21 all other safety and design basis assumptions.

22 DOE requires that each nuclear

1 facility operate within the constraints formed
2 by its safety and design basis. This ensures
3 that each facility is operated safely. For
4 WTP this means that the final documented
5 safety analysis must incorporate each aspect
6 of the QRA with the potential to impact the
7 safety and design basis.

8 The staff believes that this will
9 be a complicated undertaking made even more
10 difficult by the fact that WTP is a one-of-a-
11 kind facility. There are no DOE standards or
12 requirements for the use of QRA nor
13 expectations for controlling the assumptions
14 from the QRA in the safety basis. It is not
15 clear whether DOE intends to develop a set of
16 order requirements and standards applicable to
17 the use of QRA before allowing its use in the
18 WTP.

19 BNI and its subcontractors must
20 still complete the calculations and reports
21 that form the design strategy. Many of these
22 calculations will require review by the HIRT

1 to determine whether their findings have been
2 resolved.

3 DOE and BNI have developed a very
4 aggressive schedule for resolution of the HIRT
5 findings. It is not clear what involvement
6 the HIRT has had in the proposed resolution of
7 their findings. The staff believes that the
8 actions needed to resolve many of the findings
9 will require considerable effort and are
10 technically difficult.

11 Several findings will likely
12 require additional testing. The staff
13 believes the following findings in particular
14 will demand considerable effort and will be
15 difficult to accomplish in the proposed
16 schedule.

17 Finding 2.4, the need to consider
18 plant level events in the QRA models, requires
19 the QRA to be expanded to address plant-wide
20 events that contribute to event duration.

21 Finding 2.7, the enhanced treatment of
22 phenological uncertainties addresses

1 uncertainties regarding the gas pocket
2 formation and hydrogen combustion.

3 Lastly, combining two findings,
4 3.6 and 3.7, regarding simulant selection for
5 gas testing, the HIRT found that the simulant
6 used to perform gas testing was not properly
7 documented and that the range of yield
8 stresses, one of the most important parameters
9 used in gas testing and QRA calculations, must
10 be revised or justified in the terms of
11 expected behavior of the waste.

12 The staff believes that these
13 latter two findings if not adequately
14 addressed will prevent the QRA's use. The
15 calculations to determine the bubble size form
16 the basis for determining the frequency and
17 severity of hydrogen explosions.

18 The staff does not believe that
19 the simulant, Laponite, used by BNI to perform
20 bubble tests, adequately represents the waste
21 found in WTP and that additional testing is
22 required to properly resolve these findings.

1 In its response to the HIRT
2 finding BNI acknowledge that additional
3 testing might be needed. However, DOE and BNI
4 did not appear to have allotted the time
5 needed to conduct the testing and adequately
6 resolve the issue.

7 DOE is committed to resolve HIRT
8 findings and plans to include HIRT members in
9 the resolution process. The Board staff
10 believe this is an important facet of
11 finalizing the design basis for hydrogen
12 controls.

13 That completes my prepared
14 testimony and we would be happy to try to
15 answer any Board questions.

16 CHAIRMAN WINOKUR: Thank you, Mr.
17 Kasdorf.

18 Do Board members have any
19 questions of the staff? If not, I would like
20 to invite the panel of witnesses from the
21 Department of Energy, its contractor
22 organizations, and its experts to take their

1 seats. I would like to introduce them.

2 Dr. Ines Triay is the Assistant
3 Secretary of Energy for Environmental
4 Management. Mr. David Brockman is the Manager
5 of DOE's Office of River Protection. Mr.
6 Knutson is the DOE Project Manager for the
7 Waste Treatment Plant. Mr. Russo is the
8 Bechtel Project Director for the Waste
9 Treatment Plant.

10 Mr. Ashley is the Bechtel
11 Engineering Director for the Waste Treatment
12 Plant. Mr. Sain is the URS Executive Vice
13 President for Performance Assurance and
14 Operations. Ms. Busche is the URS Nuclear
15 Safety Manager for the Waste Treatment Plant.

16 Dr. Joseph Shepherd is Professor
17 of Aeronautics and Mechanical Engineering at
18 the California Institute of Technology. He
19 provided consulting experience to DOE on
20 detonations and deformations.

21 Does any member of the panel wish
22 to submit testimony at this time? We have a

1 lot of material to cover at this hearing. The
2 Board has chosen its panelists carefully and
3 request that panelists alone answer questions
4 that are directed to them to the best of their
5 ability. If the panelists would like to take
6 a question for the record, their answer to
7 that question will be entered into the record
8 of this hearing at a later time.

9 With that, we will begin the panel
10 session with a question from Ms. Roberson.

11 VICE CHAIR ROBERSON: Good
12 morning. My first question is to you, Mr.
13 Ashley. Can you provide for us an estimate of
14 a flammable gas that will evolve in the WTP on
15 a daily basis and what fraction of that will
16 be in piping and inline components?

17 MR. ASHLEY: We can provide that
18 for the record but I cannot. In terms of
19 total volume of flammable gas we do evaluate
20 dependent upon the feed stream. It is very
21 dependent upon the feed stream and it's very
22 dependent upon the locations and the

1 conditions and the temperature.

2 One thing that I would like to
3 clarify in the previous testimony from Mr.
4 Kasdorf, he indicated that the predominant
5 mechanism for generation of the flammable
6 hydrogen gas in the Waste Treatment Plant was
7 radiolysis. In fact, the predominant
8 mechanism is thermolysis on the side of the
9 process where organics are present. That is
10 an important clarification.

11 VICE CHAIR ROBERSON: Let me ask
12 you the estimate that you will provide for the
13 record that you are using in your design does
14 it include both gases that are entrained in
15 the waste when the waste enters the pipe and
16 gas that is generated during the time that
17 it's in the pipe?

18 MR. ASHLEY: Our estimates do
19 include the total gases that are expected to
20 be present in all phases of the process.

21 VICE CHAIR ROBERSON: So it does
22 include entraining?

1 MR. ASHLEY: That's correct. It's
2 the gases that are generated and the gases
3 that are present inline, the gases that are
4 generated and the gases that are present in
5 the vessels.

6 VICE CHAIR ROBERSON: And how do
7 you -- what is your basis for the amount of
8 gas that is entrained? What is your basis of
9 estimate for that?

10 MR. ASHLEY: The basis of estimate
11 are correlations done from studies in the tank
12 farms. There is a specific correlation that
13 has been reviewed previously by the Defense
14 Board staff. That hydrogen generation
15 correlation is used in the Waste Treatment
16 Plant.

17 VICE CHAIR ROBERSON: Okay. The
18 assumed gas composition is based on inputs
19 from the Hu correlation like the concentration
20 for the Hu nuclei. Right?

21 MR. ASHLEY: The Hu correlation.

22 VICE CHAIR ROBERSON: Right, Hu.

1 I'm from Alabama. The HIRT recommended
2 accounting for nitrogen gas and nitrous oxides
3 as a function of waste processing. Will the
4 project develop new correlations to account
5 for the generation of nitrogen and nitrous
6 oxide?

7 MR. ASHLEY: The nitrous is
8 assumed. The most energetic of the potential
9 hydrogen events is the combination of hydrogen
10 with nitrous. The nitrogen is a diluent and
11 the questions that were asked by the HIRT was
12 the diluent actually could cause the
13 generation or the creation of a larger bubble
14 which could actually affect the
15 characteristic, though a less energetic event
16 could actually be a longer run-up to the
17 event. In essence what that means is that the
18 ultimate event could potentially be larger so
19 that is being evaluated as part of response to
20 the HPAV IRT [Hydrogen Pipes and Ancillary
21 Vessels Independent Review Team] finding.

22 VICE CHAIR ROBERSON: Go ahead.

1 CHAIRMAN WINOKUR: I just want to
2 go back to a previous question that Ms.
3 Roberson asked. You are going to understand
4 the amount of hydrogen both in entrainment
5 into the vessels that's coming into the
6 facility. Correct?

7 MR. ASHLEY: Correct.

8 CHAIRMAN WINOKUR: That will
9 depend upon what's in the batch that's coming
10 in to be processed.

11 MR. ASHLEY: That's correct.

12 CHAIRMAN WINOKUR: So consequently
13 there is a need at the tank farms to be able
14 to understand what is being delivered to the
15 Waste Treatment Plant.

16 MR. ASHLEY: Correct.

17 CHAIRMAN WINOKUR: And how well
18 can you determine that what's coming in in a
19 given batch? What are you shooting for, five
20 percent, 10 percent, 15 percent?

21 MR. ASHLEY: There is a
22 requirement in ICD-19 [Interface Control

1 Document 19]. The batch is sampled. The
2 batch is tested to determine what the hydrogen
3 generation rate will be for the batch as it
4 comes into the WTP. That then will be
5 verified against the waste acceptance criteria
6 that has been a control in the ICD-19 and
7 remains a control in the ICD-19.

8 CHAIRMAN WINOKUR: So after this
9 whole process is done you'll determine a waste
10 acceptance criteria in terms of the hydrogen
11 generate that you can tolerate in this QRA
12 methodology and analysis?

13 MR. ASHLEY: No. If you think
14 about it, what we are doing is a conservative
15 analysis based on hydrogen generation rates.
16 We don't intend to have a specific
17 revaluation. It's an incoming waste
18 acceptance.

19 It will be compared against the
20 criteria that has been applied through the
21 QRA. It is an acceptance criteria for the
22 waste. It doesn't rely on getting that

1 specific batch prepared, measuring the
2 hydrogen generation rate, and then reanalyzing
3 through a QRA.

4 It is done in advance. It is done
5 based on conservative hydrogen generation
6 rates through the QRA. The waste acceptance
7 criteria will ensure that those requirements
8 are not exceeded.

9 VICE CHAIR ROBERSON: Okay. I'm
10 not sure I understood your response. Will you
11 need new correlations or not?

12 MR. ASHLEY: We will not.

13 VICE CHAIR ROBERSON: Okay. Is
14 the bubble logic currently used in the QRA a
15 conservative estimate of the hydrogen in the
16 pipe hazard?

17 MR. ASHLEY: The bubble logic and
18 the way the bubbles are considered is
19 conservative. There were questions that were
20 asked through the HPAV IRT in terms of
21 evaluating the radiology to determine if our
22 experiments, in fact, provide those

1 conservative representations. We are in the
2 process of evaluating that but the way we
3 treat the bubble and the shape of the bubble
4 is conservative.

5 VICE CHAIR ROBERSON: Mr. Ashley,
6 the testing conducted by your contractor used
7 Laponite to develop the QRA. Right?

8 MR. ASHLEY: That's correct.

9 VICE CHAIR ROBERSON: The HIRT
10 had two findings, F36 and F37 --

11 MR. ASHLEY: That's correct.

12 VICE CHAIR ROBERSON: -- that
13 question the basis for the selection and
14 suggested additional testing might be
15 required. In your closure plan you indicate
16 that the waste properties used in the QRA will
17 be consistent with the documented properties
18 for the route being evaluated.

19 MR. ASHLEY: That's correct.

20 VICE CHAIR ROBERSON: What is the
21 source of the documented properties?

22 MR. ASHLEY: Once again, if you

1 look at the flow sheet, we have various
2 stages. We have the received waste. We
3 understand the radiological properties of the
4 received waste. Then as we process the waste
5 we have controls on how we process that waste.

6 As it transitions from, in effect,
7 a Newtonian behavior to a non-Newtonian
8 behavior after leach ultra-filtration, which
9 is concentration and wash. The properties
10 will be consistent in the route with the
11 expected properties. The reason for Laponite
12 is Laponite exhibits a non-Newtonian.

13 Another reason for the use of
14 Laponite is very simple; it's clear. If
15 you're measuring and trying to observe bubble
16 formation, you need a clear simulant. If we
17 went to a non-Newtonian simulant that was
18 based on clays, for example, you couldn't
19 observe bubble formation. It's very simple,
20 the Laponite. It's a non-Newtonian fluid and
21 it allows for observations that were necessary
22 to measure bubble formation when gas is

1 released.

2 VICE CHAIR ROBERSON: Is the 9805
3 report the same documented properties for
4 mixing? Are the documented properties you're
5 talking captured in the 9805 report?

6 MR. ASHLEY: The radiological
7 properties are going to be dependent upon the
8 system plan that's provided by the tank farm
9 for each of the feeds that come in.

10 VICE CHAIR ROBERSON: Okay.

11 MR. ASHLEY: I received a note and
12 I do need to clarify we do not estimate the
13 dissolved or entrained hydrogen. We measure
14 the gas that evolves from the waste.

15 VICE CHAIR ROBERSON: Okay.

16 MR. ASHLEY: I do want to clarify.
17 I did misstate.

18 VICE CHAIR ROBERSON: Let me just
19 ask you. With that in mind then, your
20 estimate is conservative. How do you validate
21 that conservatism with that correction in
22 mind?

1 MR. ASHLEY: The conservatism in
2 terms of the hydrogen generation rates have
3 been evaluated relative to the correlation,
4 the Hu correlation, and the processes of
5 hydrogen generation to determine exactly what
6 the margin is in our estimation of hydrogen
7 generation versus what the expected is from
8 both the hydrolytic and thermolytic reactions.

9 That was reviewed in substantial
10 detail by one of the experts that was on the
11 HPAV Independent Review Team also confirming
12 the conservatism. In fact, in the HPAV one of
13 the topical reports that's part of the HPAV
14 IRT report it specifically plots that
15 conservatism in the hydrogen generation rate
16 versus what the expected actual generation
17 rates are.

18 VICE CHAIR ROBERSON: Let me just
19 make sure I don't stumble over this and make
20 sure I understand. In your response to the
21 Board and the response in the closure plan to
22 the HIRTS issue the documented properties, as

1 I just understood you to say, will be the
2 result of a flow sheet and testing provided by
3 the tank farm.

4 MR. ASHLEY: Our flow sheet when I
5 talk about the properties and how the
6 properties of the waste stream change as they
7 go through the WTP, the tank farm doesn't
8 control that. The tank farm is controlling
9 the properties of the waste as we receive it.

10 Once we start to process that
11 waste through our leach ultra-filtration
12 concentration and wash process those
13 radiologic properties do change. In terms of
14 bubble formation specifically depending upon
15 if we're in the post-leach ultra-filtration,
16 which is concentration and wash side, the
17 radiological properties are non-Newtonian, or
18 primarily non-Newtonian.

19 The Newtonian side obviously there
20 is a different mechanism for the release of
21 gas into those systems. The hold up of
22 bubbles in a non-Newtonian slurry are

1 different. As I stated, the use of the
2 Laponite has non-Newtonian properties and
3 that's why the experiments were done with
4 Laponite.

5 VICE CHAIR ROBERSON: Okay.
6 Maybe I'm just not communicating or maybe I
7 don't understand what you're saying. You
8 indicate that the waste properties used in the
9 QRA will be consistent with the documented
10 properties for the route being evaluated.

11 MR. ASHLEY: Correct.

12 VICE CHAIR ROBERSON: Okay. What
13 are the properties and where are they coming
14 from?

15 MR. ASHLEY: The properties are
16 coming from our flow sheet. In other words,
17 the non-Newtonian properties are the waste so
18 post-leach we have a range of expected non-
19 Newtonian properties from the sheer stress of
20 30 pascals to a viscosity of 30 centipoises
21 down to a low range of properties that is more
22 in the range of six pascals, six centipoises.

1 That is the range of expected
2 properties on the non-Newtonian side of our
3 process. That is important in terms of the
4 generation of gas and the release of the
5 bubbles within that slurry and how the bubbles
6 form.

7 VICE CHAIR ROBERSON: So really
8 we're talking the same properties we discussed
9 at length in the mixing session yesterday?

10 MR. ASHLEY: That's correct.
11 That's correct because, you know, our piping
12 -- this is a batch process. Our piping
13 transfers from one batch or one unit operation
14 to the next.

15 As we concentrate slurries we are
16 creating a non-Newtonian slurry. We transfer
17 that non-Newtonian slurry down to the next
18 unit operation in the process. Obviously the
19 mixing system then has to deal with that waste
20 that has those specific properties.

21 VICE CHAIR ROBERSON: Okay.
22 Thank you.

1 CHAIRMAN WINOKUR: Let me
2 understand something about what you just said
3 about the mixers. One of things we didn't get
4 much of an opportunity to discuss yesterday
5 were these pump-out experiments that you had.
6 A little bit we discussed it.

7 I think when you were doing the
8 pump-outs you noticed that you had in the
9 batches initially a lot of clearing of some of
10 the heavier dense particles and the fissile
11 materials and so on and so forth came out in
12 like the first quarter batch. Right?

13 Can you account for that in the
14 piping in terms of what's going into the
15 piping in terms of hydrogen generation rates
16 that you might be getting? You're not going
17 to get a uniform feed from the vessels. You
18 could get a very different kind of feed is
19 what I heard yesterday. How do you account
20 for that?

21 MR. ASHLEY: Once again, it is
22 important to separate the size of the process.

1 What we talked about and what Dr. Dickey
2 talked about, the tests that we ran were on
3 the Newtonian mix. In effect, that's one of
4 our most challenging vessels is what we call
5 the HLP-22 [High-level Waste Lag Storage and
6 Feed Blending Process System] vessel.

7 That's the feed receipt vessel.

8 That comes in as a Newtonian mix. Non-
9 Newtonian is similar to your paint. It's
10 similar to ketchup. The Newtonian mix is
11 basically particles in water or particles in
12 a relatively low velocity fluid.

13 When we talked about the segregation
14 of the fast settling particles and the
15 distribution of those particles in that vessel
16 with the larger, faster settling particles
17 being more towards the bottom of the vessel,
18 we're talking about these Newtonian vessels
19 like HLP-22.

20 Now, as we move to the non-Newtonian
21 side, and we did a much larger scale of non-
22 Newtonian testing at PNNL [Pacific Northwest

1 National Lab] that was done in the '03 to '05
2 time frame to really look at what the best
3 design for the mixing systems in non-
4 Newtonian. Very different.

5 What you see is you see those
6 vessels are more homogeneously mixed. Once we
7 do shear the non-Newtonian fluids, though,
8 there is the potential for larger or fast
9 settling solids to settle. However, the
10 properties of the non-Newtonian fluid which
11 have essentially being plastic properties end
12 up with apparent velocity that actually
13 reduces the settling rate of those large
14 particles.

15 We have evaluated that on the mixing
16 side as well so that the behavior in the mixed
17 vessels on the Newtonian side is different
18 than the behavior of the vessels on the non-
19 Newtonian side of the process.

20 CHAIRMAN WINOKUR: My question was
21 really a lot simpler. Thank you. I just want
22 to know -- I mean, you're mixing these things

1 in the tanks and you just told me you measured
2 the hydrogen gas to get a measure of what the
3 hydrogen generation rate is going to be.

4 When you think about the tank farms
5 you have to ask questions about how uniform is
6 it the batch you're going to be sending over.
7 Are you adequately mixing it in the tanks. Do
8 you really have a representative sample. I'll
9 put that aside for a second.

10 Now, you get into the vessels. We
11 know that these vessels are not going to
12 uniformly mix the waste. We know its
13 stratified, especially for the denser and the
14 fissile materials. When you start to transfer
15 waste into pipes, you don't really have an
16 average value of hydrogen generation weight
17 going into those pipes. Do you? I mean, the
18 generation rate could be more depending upon
19 the batch you transfer or less. I'm just
20 trying to get a sense if that's accounted for.

21 MR. ASHLEY: It's correct that the
22 slurry content could change from the top of

1 the vessel. As we start to transfer the fluid
2 in the vessel it could change with a higher
3 concentration of solids as we pump out the
4 lower portion of the vessel actually, which is
5 the first quarter batch that comes out. Then
6 obviously a lower concentration of solids as
7 we get to the top of the vessel.

8 I think what you find are the
9 smaller particles tend to mix more completely.
10 Even the denser smaller particles, a 10 micron
11 particle of plutonian oxide we actually find
12 mixes fairly well. Smaller particles tend to
13 mix much better than the larger heavier
14 particles as we talked about yesterday.

15 We believe there is sufficient
16 conservatism in the HGR [Hydrogen Generation
17 Rate] rates that that stratification that we
18 expect in these vessels is accounted for.

19 CHAIRMAN WINOKUR: All right.
20 That's what I was trying to get to. You're
21 saying you've accounted for the fact that when
22 each core -- when the batches are transferred

1 there may be differences in hydrogen
2 generation rate. That's accounted for and
3 it's conservatively accounted for.

4 MR. ASHLEY: There could be
5 differences. Just to give you also
6 perspective, I'm being flooded with note cards
7 --

8 VICE CHAIR ROBERSON: Must be a
9 sign of something.

10 MR. ASHLEY: To give you a
11 perspective, Ms. Roberson did ask what
12 quantity of hydrogen are we talking about. We
13 are talking about .1 milliliter of hydrogen
14 per liter of waste per hour just to give you
15 a perspective on quantity.

16 MEMBER BADER: Let me help you with
17 this.

18 CHAIRMAN WINOKUR: Mr. Bader has a
19 question.

20 MEMBER BADER: Mr. Ashley, you must
21 be saying something highly controversial.
22 Would you like to either call a friend or poll

1 the audience?

2 MR. ASHLEY: These are my helpers.
3 They are providing me information.

4 VICE CHAIR ROBERSON: Okay. Dr.
5 Shepherd, thank you for joining us today.
6 Welcome.

7 DR. SHEPHERD: Good morning.

8 VICE CHAIR ROBERSON: Good morning.
9 You conducted a review of BNI's calculations
10 and modeling of a gas explosion phenomena.
11 What specific concerns or issues did you
12 provide to the project or identify to the
13 project?

14 DR. SHEPHERD: Thank you. Yes. I
15 conducted many reviews of many documents. I
16 actually anticipated this and tried to count
17 them. I can't give you an accurate number.
18 I think it was somewhere between the order of
19 50 and 100 documents. The number of formal
20 reviews I submitted are somewhat smaller.

21 My concerns range all the way from
22 details of symbols and equations to the

1 overall approach to the analysis of how data
2 is being used, how computer simulations have
3 been validated. We spent substantial amount
4 of time early in the program in looking at
5 just what the approach was to analyzing
6 explosions.

7 VICE CHAIR ROBERSON: I understand
8 there is a broad range. For example, in a
9 letter to DOE on March 27th of 2010 you raised
10 a specific set of issues. Could you describe
11 those specifically?

12 DR. SHEPHERD: That was dealing with
13 some calculations that were ongoing. Those
14 calculations are still ongoing. The issues
15 there had to do with -- I believe what I need
16 to do actually is look at what that was. I
17 think that's in the book here.

18 VICE CHAIR ROBERSON: Absolutely.

19 CHAIRMAN WINOKUR: We would be happy
20 to receive that for the record,.

21 DR. SHEPHERD: It's fairly
22 straightforward so all I have to do is find my

1 dog-eared corner here and then I can talk
2 about that. Where did it go? I noticed that
3 you had a special session section here just
4 for me. So which question was that? Help me
5 out here.

6 VICE CHAIR ROBERSON: It was March
7 27.

8 DR. SHEPHERD: Right. I guess what
9 I would like to do is then respond to that for
10 the record since I don't have it in front of
11 me.

12 VICE CHAIR ROBERSON: Okay. We'll
13 probably ask you questions from that since
14 we've seen it but I think that is perfectly
15 fine. Go ahead. Let me just ask you a few
16 specific questions and I'm sure my colleagues
17 will have others as well.

18 Dr. Shepherd, you reviewed the
19 design criteria for the design of the piping
20 and inline components potentially subjected to
21 hydrogen explosions. Do you based upon your
22 review believe that the criteria are adequate

1 to protect ductile failure of a pipe in the
2 case of inline component failure of the
3 primary boundary?

4 DR. SHEPHERD: I think it's
5 important here to distinguish that there are
6 a number of different components in the WTP.
7 There's piping.

8 VICE CHAIR ROBERSON: Um-hum.

9 DR. SHEPHERD: There are components
10 such as valves and pumps and then there are
11 pressure vessels. Which particular pieces are
12 you referring to, Ms. Roberson?

13 VICE CHAIR ROBERSON: I'm asking
14 you in your opinion do the criteria applied to
15 inline components provide the same level of
16 assurance as the piping design criteria?

17 DR. SHEPHERD: What I believe is
18 that those criteria are appropriate. The ones
19 that have been developed are broadly
20 applicable to the entire facility, but
21 particular cases need to be examined and that
22 is something that I've encouraged the DOE to

1 do. The most focus has been on piping to date
2 and piping systems. I've encouraged the DOE
3 to look at the components such as valves,
4 pumps, so forth, separately. I know they have
5 a separate program looking at the vessels.

6 VICE CHAIR ROBERSON: Okay. Let me
7 ask you a connected similar question. In your
8 opinion are the calculations and models used
9 to predict a pipe's response to a gas
10 explosion adequate for predicting plastic
11 deformation in the piping system at WTP?

12 DR. SHEPHERD: My answer is a
13 qualified yes because we always have to
14 discuss what the extent of the plastic
15 deformation is that is being considered and
16 for modest amounts of plastic deformation the
17 types that are being anticipated as being
18 acceptable I believe that they are.

19 VICE CHAIR ROBERSON: Do you
20 believe in your expert opinion that BNI's
21 overall approach allows them to accurately
22 predict the amount of plastic deformation?

1 DR. SHEPHERD: I think it's
2 important to understand that we are not
3 talking about making accurate predictions
4 because we don't actually have inputs which
5 would allow us to do that.

6 If we had a definite loading
7 function and we said this is the loading
8 function, I believe that the methods that they
9 re developing are appropriate for that,
10 although that has not been the focus of the
11 program at this point to develop a highly
12 accurate plastic deformation prediction tool,
13 nor do I believe it's necessary to do so.

14 We are doing safety analysis and in
15 safety analysis what you're concerned with is
16 making sure that you have bounding
17 calculations. I believe that they are
18 developing methods which are appropriately
19 bounding.

20 VICE CHAIR ROBERSON: Okay. Let me
21 ask you, the members of HIRT, which I assume
22 you've seen their report. I believe you

1 provided insight.

2 DR. SHEPHERD: Yes.

3 VICE CHAIR ROBERSON: They observed
4 that the design criteria applied to the piping
5 system were adequate assuming that the inputs
6 into the analysis, i.e., the outputs of the
7 QRA, are accurate. Do you agree with that?

8 DR. SHEPHERD: Yes.

9 VICE CHAIR ROBERSON: I have just a
10 couple of additional.

11 CHAIRMAN WINOKUR: Just give me an
12 intuitive feel for things. I was a scientist
13 once before I got on this Board and did
14 experiments and things. How complicated a
15 problem is this? How tough a problem is it to
16 be able to -- you know, we have to figure out
17 what's actually going on, figure out how these
18 bubbles are formed, get an idea about
19 detonation events. How hard a problem is
20 this? Is this pretty well known in industry
21 what we're doing here?

22 DR. SHEPHERD: You know, the

1 individual parts of it have been studied in
2 great detail and so there are many folks who
3 have made a living in academia and industry at
4 looking at the various bits and pieces. So,
5 for example, generation of gases due to
6 radiolysis thermolysis; the motion of viscal
7 elastic material and pipes; various aspects of
8 deflagrations and detonations.

9 There are entire journal symposia
10 devoted to these things. The subject of
11 detonation inside of pipelines is something
12 that I've been working on for the last 20
13 years. We have a substantial technical base
14 on the individual aspects of this. What makes
15 this problem interesting, difficult, and
16 challenging is putting together a wide range
17 of these things.

18 The modern kind of buzz word that
19 folks use in the academic community is that
20 it's a multi-physics problem. You have a lot
21 of things going on at different scales with
22 different physical phenomena. Putting those

1 together in a way that it can be used as a
2 design tool by an engineering firm, that's the
3 thing that makes it challenging.

4 You're not going to hand a handful
5 of scientific papers to the engineers and say,
6 "Ah, there you go. Distill this with some
7 down and get some simple rules out of it and
8 you're done." What it takes doing is sorting
9 through defining what are the most important
10 phenomena that need to be addressed where you
11 can live with uncertainties because you're
12 always going to have uncertainties in a large
13 complex system where you need to really
14 sharpen up your tools and have an
15 understanding.

16 The challenges have been to bring
17 together all these desperate disciplines and
18 also think about it in terms which are terms
19 of safety. Quite frankly, the word risk is a
20 very important word here assessing the risk.
21 How do all of these different physical
22 phenomena come into creating this thing that

1 we call risk.

2 CHAIRMAN WINOKUR: Are you familiar
3 with situations in industry where people have
4 actually calculated what these probability
5 distributions would be for the frequency and
6 the magnitude of detonations in the kind of
7 situation that we're dealing with here?

8 DR. SHEPHERD: Yes. The chemical
9 industry, particularly the high hazard
10 chemical industry that is involved with
11 working with high-pressure ethylene.
12 Generating polyethylene is a good example.
13 That's an activity where you have potential
14 explosive gases and very high pressure,
15 complex petrochemical plants.

16 We had an example recently that
17 happened in the Gulf of Mexico where we had a
18 very serious accident that happened at Deep
19 Water Horizon. There were accidents that have
20 happened on off-shore dwelling platforms.

21 There was a very intensive effort
22 that took place in looking at the platforms in

1 the North Sea starting with the Piper Alpha
2 explosion in the late 1980s. A very intensive
3 effort in the European community of looking at
4 siting high-hazard chemical plants in highly-
5 populated areas.

6 Various organizations like TNO
7 [Netherlands Organisation for Applied
8 Scientific Research] in the Netherlands have
9 played a very active role in that. In the
10 chemical process industry, in fact, there is
11 a whole groups of people. The Center for
12 Chemical Process Safety is one of those. It
13 comes out of the AIChE [American Institute of
14 Chemical Engineers] that is involved with
15 that.

16 CHAIRMAN WINOKUR: Do these
17 applications allow defamations of the pipes?
18 Is that a typical thing to do?

19 DR. SHEPHERD: One of the things
20 that you have to decide is you have to decide
21 how much you are going to place emphasis on
22 your design case and what are going to be

1 exceptions.

2 What are things that are going to be
3 very unlikely things that are going to happen
4 that you may wish to accommodate through
5 plastic deformation. A very typical way to
6 think about this kind of problem is risk is a
7 combination of consequence and likelihood. At
8 the same time many commercial organizations
9 and also government organizations are thinking
10 about containing cost.

11 Also the speed with which a plant
12 can be designed Sometimes you find in that
13 space of risk that there may be some very
14 highly unlikely events. As long as the
15 consequences of those are not too high, you
16 might allow plastic deformation to occur.

17 CHAIRMAN WINOKUR: But they don't
18 typically allow for plastic deformation? It's
19 an incredible event you're telling me or an
20 extremely unlikely event. Is that what I
21 heard?

22 DR. SHEPHERD: So we have to be

1 careful about this because, in fact, plastic
2 deformation is allowed routinely in certain
3 types of motions within the piping code.
4 Something to be clear about here is that
5 plastic deformation is not a terrible thing
6 and often you have to allow some amount of
7 what is called small-scale yielding to occur.

8 Otherwise, it wouldn't be possible
9 to put it together. It's a very large system
10 with large dimensions. Everything is not
11 going to fit quite right and you have thermal
12 expansion when things move around.

13 If you have deformation that occurs
14 through beam bendings, if you have a pipe and
15 the pipe is being bent like a beam like this,
16 you can accommodate plastic deformation and
17 the piping code actually allows for some of
18 that. The question really is what is the
19 extent that you are going to allow.

20 I think as long as that extent does
21 not affect your safety basis, I think it's
22 perfectly okay to allow it as long as you are

1 very carefully understanding what the basis is
2 for the interest of that and that's where the
3 QRA comes in.

4 CHAIRMAN WINOKUR: What is a typical
5 extent and percent of deformation, for
6 example, that you would allow?

7 DR. SHEPHERD: You can allow several
8 percent deformation particularly in piping on
9 a regular basis.

10 CHAIRMAN WINOKUR: Okay.

11 VICE CHAIR ROBERSON: I just have
12 one more question for you, Dr. Shepherd.

13 DR. SHEPHERD: Yes.

14 VICE CHAIR ROBERSON: You also
15 reviewed the testing program for Southwest
16 Research. Did you raise any concerns about
17 the quality of data utilized in that testing
18 program?

19 DR. SHEPHERD: I had input into
20 various aspects of that program. One of the
21 things that I also did was review the data
22 after it was generated. I did have some

1 concerns. I think in all of these test
2 programs that one of the things in my own
3 program, and we do the same thing, we have to
4 very carefully vet the data.

5 You have to understand is what we're
6 looking at something that's physical or are
7 there artifacts. One of the things to keep in
8 mind is when you make measurements with gauges
9 like strong gauges and you have very large
10 strains so basically what you're doing is
11 you've got a little piece of material that's
12 glued onto your pipe and when the pipe moves,
13 and the pipe is moving only really microns is
14 what we're measuring, very small motions, but
15 these are very sensitive gauges.

16 It's a beautiful little thing. When
17 it's used properly it tells us what the
18 strains are. When you start to get large
19 strains, then the motion of that little glued
20 on piece of foil is not necessarily going to
21 follow the pipe.

22 Over time that connection, that

1 glued connection that we basically put on
2 there with Super Glue, can become degraded so
3 you have to be careful is that the signal that
4 you're looking at really reflective of the
5 actual strains inside of the material.

6 I had some concerns about some of
7 the signals and they have addressed those.
8 They have looked at those and they have done
9 a careful examination of those. In fact, some
10 of those strains are not going to be used in
11 their evaluation of the data.

12 VICE CHAIR ROBERSON: You want to
13 ask something else?

14 CHAIRMAN WINOKUR: Mr. Brown is
15 going to have some questions but just before
16 that one question from Mr. Bader.

17 MEMBER BADER: Dr. Shepherd, you
18 were making comparisons to the chemical
19 industry and drawing value from that. Are
20 those facilities easily inspected for
21 excessive deformation?

22 DR. SHEPHERD: Sometimes. Sometimes

1 you have components that are inaccessible. In
2 those situations you usually create a
3 different set of rules. For example,
4 analogous to what you have, the difference
5 between the hot cells and the black cells.

6 MEMBER BADER: Staying with the hot
7 cells, how would you compare the assessability
8 for inspection and repair in the hot cells
9 with inspection and repair in assessable
10 facilities in the chemical industry?

11 DR. SHEPHERD: Having never actually
12 worked in a hot cell I guess I would have to
13 defer with someone with more operating
14 experience.

15 MEMBER BADER: Would you believe
16 the presence of high radiation fields might
17 inhibit that?

18 DR. SHEPHERD: Obviously you're not
19 climbing down in there with a flashlight and
20 a micrometer looking at it.

21 MEMBER BADER: Also you mentioned
22 you're dealing with multi-physics problems,

1 desperate disciplines, and trying to assess
2 the overall risk. When you combine that with
3 the concerns about doing inspection and repair
4 in radiation fields, do you believe that would
5 call for an extra measure of conservatism?

6 DR. SHEPHERD: I think that you have
7 to weigh all of those things in deciding where
8 you are going to come down in terms of how
9 much conservatism you use.

10 MEMBER BADER: I'm asking for your
11 opinion as to whether you believe an extra
12 measure of conservatism would be a prudent
13 thing to do.

14 DR. SHEPHERD: I think certainly we
15 would all agree that when we treat these
16 facilities with these special nuclear
17 materials and the issues that you've raised
18 and the other issues that we know exist here
19 like criticality, certainly an extra measure
20 of attention to these details is important.

21 MEMBER BADER: I think that was a
22 yes. Is that correct?

1 DR. SHEPHERD: I believe it's
2 important to pay very careful attention to all
3 of these matters when you go through it.

4 MEMBER BADER: I'll take that as a
5 yes. Thank you, Peter.

6 CHAIRMAN WINOKUR: Ms. Roberson.

7 VICE CHAIR ROBERSON: Okay. Thank
8 you. Just two or three more questions, Mr.
9 Chairman.

10 CHAIRMAN WINOKUR: Sure.

11 VICE CHAIR ROBERSON: Mr. Ashley,
12 given that it is a complicated venture as
13 described by Dr. Shepherd and evidenced by the
14 HIRT review and the interaction between the
15 project and the Board, notwithstanding the
16 Department's interest to develop this to
17 further potential, broader use in the
18 Department, and also given your concern and
19 focus on schedule and cost control that you
20 and Mr. Russo reminded us of a number of times
21 yesterday, why has BNI proposed to the
22 project, to the Department, to pursue this

1 avenue rather than the better known and well
2 established deterministic approach?

3 MR. ASHLEY: I need to start off and
4 say because I believe this is the right design
5 approach for this facility. The combination
6 of the need to ensure safety and the need to
7 ensure the operability of the facility results
8 in having to take a novel approach for a very
9 complex first-of-a-kind facility.

10 I have been involved in nuclear
11 power facility design, nuclear design for my
12 entire career. The situation that you have to
13 address are what are the unique conditions,
14 what are the unique hazards associated with
15 each individual process or each individual
16 design.

17 I believe that we have done that.
18 This provides us the opportunity to work
19 towards the best design for the facility. Our
20 ultimate goal we are not just designing a
21 facility and leave. I like to leave every
22 facility knowing that I have left the operator

1 with the best possible facility for them to
2 complete their part of the mission. This is
3 a methodology that we believe is very robust.

4 Assures that we have high confidence
5 that we maintain the primary boundary of this
6 piping so that it can fulfill the mission. We
7 believe that this criteria is consistent with
8 methodology that has been applied in the
9 nuclear industry in the past.

10 VICE CHAIR ROBERSON: Thank you.

11 MR. RUSSO: Ms. Roberson, if I can
12 add just something from my perspective. When
13 I came on the project the second question I
14 asked after I learned everything I could about
15 mixing and M3 was the very question you asked.

16 Basically I was convinced after a
17 great deal of discussion with Greg, and some
18 with Dr. Shepherd and others, what Greg is
19 saying is absolutely correct. Even though
20 it's not necessarily the best thing for
21 schedule, it is the best thing for the co-
22 located worker.

1 Also, from the perspective of my
2 experience in the chemical industry, although
3 pleasure excursions here are not something
4 that we would ever anticipate or desire or
5 want, in the chemical industry the pressures
6 and temperatures they operate at you see the
7 results on the news sometimes when the entire
8 facility and three miles around it are
9 destroyed.

10 What I've seen the petrochemical
11 industry particularly do is if they have a
12 concern they go with much heavier wall pipe.
13 When their piping runs where they think there
14 can be some kind of pressure excursion and the
15 shell job being a perfect example. That was
16 a new technology.

17 Instead of coking, taking the carbon
18 out of the bitumen they put hydrogen in so it
19 was very highly explosive process if not
20 controlled. I saw some of the heaviest wall
21 thicknesses that I had ever seen on that
22 project.

1 VICE CHAIR ROBERSON: Ms. Busche.
2 So, Ms. Busche, in the response to the Board's
3 questions, Question 5E, "Doe indicated that
4 one aspect of the change in approach from the
5 original HPAV design criteria to the new HPAV
6 design criteria was to determine if the
7 project can replace an active control or
8 barrier with passive control or barrier." I'm
9 assuming this is the preferred approach from
10 a nuclear safety perspective. You prefer to
11 have a passive control?

12 MS. BUSCHE: That is correct.

13 VICE CHAIR ROBERSON: Okay. My
14 last question to you, Mr. Ashley, with this in
15 mind you are using this tool to help you
16 determine active and passive control, again,
17 with consideration of the pressures of the
18 project. When I look at this simply, why
19 isn't increasing the pipe schedule an option?

20 MR. ASHLEY: It is.

21 VICE CHAIR ROBERSON: So what is
22 the balance between doing that and utilizing

1 this too? Where is that line? What is that
2 decision process?

3 MR. ASHLEY: The criteria enables
4 those decisions. For example, if the current
5 anticipated design were what we call a
6 Schedule 40 pipe, which is from a process
7 standpoint is probably the minimum pipe size
8 meaning wall thickness that we have on the
9 project.

10 If the criteria as we went through
11 the analysis and the postulated events -- and
12 I call these postulated events. These are
13 what we postulate might happen or could
14 happen. If we are unable to meet the criteria
15 for that Schedule 40 pipe, the engineer's
16 first response could be to increase the
17 schedule of the pipe to Schedule 80 pipe.

18 In the current project we have put
19 the HPAV affected pipe, that's where we could
20 potentially postulate an event in four inch
21 and under pipe, though that pipe had been
22 procured some years ago prior to the evolution

1 of how we were going to address the HPAV
2 phenomena. We put that on hold because what
3 we don't want to do is install any of that
4 pipe and preclude the opportunity to increase
5 the schedule of the pipe.

6 There are limits. The pipe has to
7 interface with other components like vessels.
8 We could go to Schedule 160 but Schedule 160
9 decreases the internal flow area of the pipe
10 and would require a more substantial redesign
11 of mechanical systems, reevaluating flows and
12 pressures, so there is a limit to the schedule
13 of pipe that we could go to. But we will meet
14 our criteria to assure that we protect the
15 pressure boundary. If to do that requires the
16 increase in pipe schedule, that's what will be
17 done.

18 VICE CHAIR ROBERSON: What I just
19 heard you say is you need this tool to tell
20 you what pipe schedule to go to?

21 MR. ASHLEY: Design criteria very
22 simply tells an engineer what material do I

1 need to meet the design, what's the geometry
2 of the material that I need to meet the
3 design. That criteria drives the design.

4 What we establish as our acceptance
5 criteria very much drives the design. The
6 design, the selection of a pipe schedule, the
7 routing of a pipe, how I support the pipe.
8 That's all driven by an acceptance criteria
9 which assures the performance of that system.

10 VICE CHAIR ROBERSON: Right. So
11 you need this tool to inform you on pipe
12 schedule selection?

13 MR. ASHLEY: I need the full sweep
14 of tools which is design criteria, which is
15 the code, which is material properties
16 associated with the code. I need to know the
17 load. As an engineer I need to know what is
18 the load that pipe is going to see. In this
19 case it's a pressure response.

20 Then I'm going to take that severity
21 and frequency of that event and then I'm going
22 to evaluate how my piping system and my inline

1 components respond to that event. I'm going
2 to determine what the stressors are in that
3 pipe and in those components. I'm going to
4 determine what the loads are on the supports.
5 It's all part of the process of design.

6 VICE CHAIR ROBERSON: I'm going to
7 let somebody else ask questions, Mr. Chairman.

8 MR. DEWEY: Ms. Roberson, if I could
9 just follow up your question for a second.

10 So, let me try and ask it a different way.

11 You're going to use this tool and you're going
12 to say this particular run of pipe that we're
13 analyzing suffers three plastic deformations
14 of less than 2.5 percent strain so that's
15 acceptable.

16 MR. ASHLEY: No, that's not the way
17 we do design. Okay. What we do is we have to
18 start with what is the event that I'm
19 designing for. Then I take that event and I
20 analyze that system to see what that system's
21 response is to that load. We don't assume
22 that we are going to be at the high end of our

1 acceptance criteria.

2 I could have an HPAV event, a series
3 of HPAV events that could result in responses
4 that are well below the yield of the material,
5 that there is no plastic strains associated
6 with that event. The criteria I must meet is
7 I must be below my acceptance criteria.

8 MR. DEWEY: Which are?

9 MR. ASHLEY: My acceptance criteria
10 in the hot cell is yield stress at .2 percent
11 strain offset which is the elastic limit.
12 That is defined as the elastic limit. In the
13 hot
14 cell --

15 MR. DEWEY: You said hot cell.

16 MR. ASHLEY: I'm sorry, black cell.

17 MR. DEWEY: Thank you.

18 MR. ASHLEY: Black cell. In the hot
19 cell it's 3 percent strain. Now, I must meet
20 the code so I must evaluate how many times
21 that event could occur or is postulated to
22 occur over the life of the facility because I

1 must evaluate the cumulative effect of
2 multiple events.

3 The rigor of this criteria is and
4 the reason that we need an estimate of
5 severity and frequency is I need to design for
6 the potential for multiple events and assure
7 that I maintain the pressure boundary of this
8 piping of that primary boundary over the life
9 of the facility.

10 MR. ASHLEY: Okay. And the "limit
11 number of events" is?

12 MR. DEWEY: It's a detailed fatigue
13 evaluation. We're limiting -- we believe an
14 appropriate limit would be three events of the
15 most severe event.

16 MR. ASHLEY: Okay. Let me try
17 again. You have a piping run for which you
18 have calculated that you will get, over the
19 life, the 2.5 percent strain event three times
20 and that would be acceptable but that will
21 cause plastic deformation.

22 MR. DEWEY: That's correct.

1 MR. ASHLEY: Why, since you've
2 already said, "We'll adjust pipe schedule
3 based on what we need," why would you not just
4 say, "We'll not allow plastic deformation at
5 all. Go ahead and increase the pipe
6 schedule?"

7 MR. DEWEY: It meets criteria. For
8 the criteria we can maintain. If it were the
9 current design of Schedule 40 that meets the
10 criteria. That is allowable. It then becomes
11 specific judgment as to whether I would want
12 to increase the pipe schedule to Schedule 80
13 but our design will meet our established
14 criteria.

15 MR. ASHLEY: And I'm still left with
16 why. If you could do it and not have plastic
17 deformation, why not?

18 MR. DEWEY: Would you take the same
19 approach in normal operating pressure design
20 for pipe that says I meet the code. I meet
21 the code allowable for normal operating load.
22 Why don't I just increase the pipe schedule to

1 the next schedule. It's not the way you do
2 design. You design to a criteria.

3 MR. ASHLEY: Correct. And in this
4 case you set a criteria that allows plastic
5 deformation.

6 MR. DEWEY: Correct.

7 CHAIRMAN WINOKUR: I have one more
8 quick question and then we're going to Mr.
9 Brown. That is when you have these plastic
10 deformation events you talk about, what is the
11 impact on the jumpers and other inline
12 connectors that the Board has expressed a lot
13 of concern about?

14 MR. ASHLEY: Inline components --
15 complex inline components are not qualified by
16 analysis. They are not qualified to a strain
17 criteria. They will be qualified by test. We
18 did demonstration tests. Demonstration tests,
19 not qualification tests.

20 In the experiments at Southwest
21 Research on PUREX connectors, for example, we
22 did see limited plastic deformation with a

1 pressure reflected DDT [deflagration
2 -to-detonation transition] during those tests.
3 I want to put into perspective when we talk
4 about three percent strain and people talk
5 about bulging pipe, the PUREX connector -- we
6 measured about 1.8 percent strain in the PUREX
7 connector.

8 It's 53 thousandths of an inch
9 diametrical. Visual inspection would be
10 unlikely to identify that level of plastic
11 strain. When you talk about bulging pipe, you
12 are generally talking about strains in the
13 range of 25, 30 percent. We're talking three
14 percent plastic strain.

15 As Dr. Shepherd mentioned earlier,
16 standard design in piping fittings
17 acknowledges there is plastic strain during
18 normal operating loads.

19 CHAIRMAN WINOKUR: I'll probably
20 come back to this a little later. I want to
21 go to Mr. Brown now.

22 MEMBER BROWN: Good morning. Thank

1 you all for being here. I'm going to continue
2 the questions which will be primarily Mr.
3 Ashley and Dr. Shepherd, although I do have to
4 ask should I call you Dr. Shepherd, Professor
5 Shepherd, Dean Shepherd? Do you have any
6 other titles that I've missed?

7 DR. SHEPHERD: Just Joe.

8 (Laughter.)

9 MEMBER BROWN: That must be a
10 California thing. I had the opportunity, this
11 is kind of a side story, to be the driver for
12 Condoleezza Rice when she went to meet Sandy
13 Berger for the first time at the White House
14 10 years ago.

15 She had never met me before and so I
16 helped her into the car and then I turned to
17 her and I said, "Should I call you Provost or
18 Dr. Rice or Professor Rice?" She said, "Just
19 call me Condi." I guess that's a California
20 thing. Just call me Joe.

21 My questions are primarily on the
22 testing program. I just want to go through

1 it. We've talked around about it but I would
2 like to try to fill in the whole picture. Let
3 me begin with Mr. Ashley.

4 We've talked about how Cal Tech and
5 Dominion Engineering and Southwest Research
6 were key elements of your testing program.
7 Were there any other significant elements of
8 the testing program?

9 MR. ASHLEY: No. Those were the
10 primary elements.

11 MEMBER BROWN: Okay. Could you
12 describe the scope of this testing program;
13 what you are trying to achieve, what it
14 involved, how long it's been going on.

15 MR. ASHLEY: My recollection, and
16 Dr. Shepherd can correct me, I think it's been
17 going on about five years. I think the
18 initial testing that Dr. Shepherd began at Cal
19 Tech was in 2005.

20 Some of the initial investigations
21 were with fairly simple systems in Dr.
22 Shepherd's laboratory looking at two-

1 dimensional systems, not just straight runs of
2 pipe, but bend systems and provided some of
3 the very important foundational work early on
4 in the program.

5 The testing at Southwest Research
6 then advanced that testing to full-scale
7 piping systems of more complex geometry
8 including some demonstration tests for some
9 inline components down at Southwest.

10 The role of Dominion Engineering in
11 the overall program in effect is as the
12 analyst because obviously Dr. Shepherd's work
13 really focused very heavily on some
14 fundamental phenomenology, what happens, how
15 these events transition from deflagrations to
16 detonations and responses.

17 Dominion's role was really
18 establishing how are we going to take this
19 data and this measured response data and
20 develop analytical tools that would allow us
21 to conservatively predict the responses of the
22 piping systems to these postulated HPAV

1 events.

2 If you think about Dominion,
3 Dominion worked in taking some of Dr.
4 Shepherd's data.

5 A lot of Dr. Shepherd's data worked
6 taking Southwest Research data, and then
7 really taking that data and developing
8 analytical models that would assure that we
9 could conservatively predict the responses
10 that we were actually measuring in these
11 piping systems in the laboratories and at the
12 larger scale down at Southwest Research.

13 MEMBER BROWN: So what you're
14 really looking at is the bounding cases for
15 this rather than what all the possibilities
16 are but basically the boundaries of the HPAV
17 uncertainties?

18 MR. ASHLEY: Well, yes.
19 Determination of uncertainty, how we would
20 address uncertainties, how well the models can
21 correlate. If the models don't correlate
22 well, how would we have to address that. All

1 the way through to how do we combine the
2 stresses.

3 There's a whole lot of technology, a
4 lot of important analytical methods in terms
5 of how stresses actually combine, stresses
6 along different axes in a pipe. How do they
7 combine to result in strains in the pipe?

8 All of that was really part of this
9 program is to be able to get to a criteria
10 that provides us the high confidence that we
11 could evaluate the responses of our piping
12 systems to these HPAV events that we then
13 could use for qualification.

14 MEMBER BROWN: Dr. Dickey yesterday
15 talked about an unexpected result of, I guess,
16 in your Newtonian vessels the stratification
17 of the heavier particles and how those were
18 dominantly taken out of the tank when you were
19 pumping out. Have you had any similar
20 surprises, if you will, in your HPAV program,
21 things that you didn't expect?

22 MR. ASHLEY: If you look down at the

1 individual responses in a piping system, there
2 were some responses that I think -- you know,
3 we worked pretty closely with Dr. Shepherd,
4 scratched our head, some things that we call
5 high frequency oscillations. We saw those
6 responses.

7 We tried to understand and make sure
8 we understood what those were. Then we had to
9 make sure that we could understand how we had
10 to evaluate those and how we had to include
11 those in the design process. Dr. Shepherd can
12 speak to it.

13 He's probably seen in the lab those
14 responses before but from the engineer
15 standpoint those were responses that I would
16 say we didn't anticipate but they were
17 important to be evaluated and included in the
18 overall design criteria.

19 MEMBER BROWN: Would you like to
20 comment on that, Dr. Shepherd?

21 DR. SHEPHERD: Yes. So this is the
22 kind of interesting, fun, academic part of it,

1 although I think it perplexes sometimes the
2 engineers how to handle these things. What we
3 were confronted with when we came into this
4 program is that the state-of-the-art in
5 evaluating detonations and piping systems was
6 pretty low. In fact, there was not really any
7 agreed upon design methodology for this, a set
8 of standardized loadings which you would use.

9 The engineering groups like Bechtel
10 come about this from the point of view that
11 this is a structural mechanics problem. If
12 you'll tell me what the loading looks like,
13 what the pressure is as a function of time
14 inside of the pipe they have very highly
15 developed methods to do structural analysis.

16 That's what Dominion is doing and
17 what Greg was referring to with their
18 analytical methods so they use these finite
19 analysis tools to calculate the response of
20 the piping and see if they can develop loading
21 methods, loading descriptions for the
22 different things that happen, deflagration,

1 detonation, transition from deflagration to
2 detonation.

3 What happen when the detonation goes
4 around the bend in the pipe. What happens
5 when it reflects off of the dead end. What
6 happened when it goes through a T. These were
7 the things that we actually did not have a
8 good grasp on in 2005 when I got started on
9 this program.

10 One of the things that this program
11 has done is really significantly advance the
12 state of the art in how to model all of these
13 features and make reliable engineering
14 predictions of the response of the pipe. Now,
15 this is a problem which is a little different
16 than what piping designers usually confront
17 because the detonation waves move pretty fast.

18 They are moving at several thousand
19 meters per second so they excite elastic waves
20 in the piping that ordinarily are not part of
21 piping design. Piping design is basically you
22 have a piece of material and it might undergo

1 seismic loading which has oscillations on the
2 order of a few hertz or tens of hertz but you
3 typically don't consider oscillations which
4 could be hundreds of kilohertz which is what
5 gets excited when the detonation wave moves
6 through.

7 It's necessary to expand how you are
8 thinking about this. It's necessary to
9 understand how you are going to account for
10 these things with your standard engineering
11 tools. There's standard piping codes that
12 they're using.

13 One of the things we had to do was
14 develop methods for how do we prescribe what
15 the forces are going to be in the standard
16 piping code ME101 that Bechtel uses for doing
17 their design. This is, as far as I know, the
18 first time that this has really been done for
19 detonations and we've come up with a set of
20 prescriptions of how to do this.

21 We progressed from the point where
22 we were absolutely ignorant about it to now we

1 can make reasonably reliable predictions. We
2 show that for fairly complex piping systems
3 that incorporated the kinds of features that
4 you have, not all of the features but most of
5 the features; three dimensionality, bends, Ts,
6 so forth, in my laboratory and at Southwest
7 Research, piping systems that were -- in my
8 lab it was 70 feet long.

9 At Southwest I think it was 200 feet
10 long, and able to show by using this kind of
11 breaking it down into components developing
12 models for each of these individual parts, we
13 can simulate the whole. In the process of
14 doing that, some of these features like these
15 high frequency oscillations, these are things
16 that are kind of unusual creatures.

17 How well are we going to need to
18 understand those to do the design? I think
19 they are things that we don't have to
20 understand particularly well because the other
21 strains and stresses which we can reliably
22 calculate, in fact, bound those things but

1 they remain as something that we don't clearly
2 understand.

3 MEMBER BROWN: Thank you. Mr.
4 Ashley, what are the uncertainties that you
5 are still trying to grapple with and resolve -
6 -

7 MR. ASHLEY: Well, I think --

8 MEMBER BROWN: -- related to the
9 testing program?

10 MR. ASHLEY: Related to the testing
11 program in terms of our ability to correlate
12 our design models with testing, there really
13 are not a substantial number of uncertainties.
14 There were some HPAV Independent Review Team
15 findings that required that we provide
16 additional justification.

17 We had, I think, good discussions
18 with their team, additional justification for
19 how we combine some stresses. The data is
20 available. We don't need additional data for
21 that.

22 The uncertainties that we are still

1 addressing have to do with the questions that
2 were asked with regard to other gases like
3 nitrogen that could cause formation of larger
4 bubbles.

5 What effect does that have on what
6 we call our run-up links as we predict what
7 the event is. I think Dr. Shepherd provided
8 good insights on how to address that. There
9 is data out there that helps support that. We
10 are completing that work.

11 I think as Mr. Kasdorf mentioned in
12 his testimony, the bubble formation and our
13 confidence in our bubble formation models are
14 conservative. There is some uncertainty there
15 that we are addressing in two ways.

16 One of the beauties of the
17 quantitative risk analysis is it allows you to
18 address uncertainties. Also we are addressing
19 those uncertainties specifically relative to
20 the phenomenology because that bubble model is
21 part of our quantitative risk analysis.

22 If you go through the HPAV

1 Independent Review Team model, I think the
2 remaining uncertainties that we need to
3 resolve before we can fully implement that are
4 well documented. Our action plan actually to
5 address those uncertainties is documented in
6 our closure plan for those both on the finding
7 side and the recommendation side.

8 MEMBER BROWN: Thank you, Mr.
9 Ashley.

10 I've got a real void here in the
11 middle of the panel. Most of my questions are
12 really to Dr. Shepherd but I don't want to
13 leave you out.

14 I would ask maybe, Mr. Knutson, how
15 involved are you in this testing program and
16 the direction of the testing program? Do you
17 review the data that they're looking at and
18 are there other questions that you've added or
19 you expect -- I mean, are you actively
20 involved in the direction of this testing?

21 MR. KNUTSON: I guess, first, thank
22 you for pronouncing my name correctly. Second

1 --

2 MEMBER BROWN: We're both
3 Scandinavians.

4 MR. KNUTSON: -- the Department of
5 Energy has technical experts that are part of
6 our project team that are engaged with the
7 testing plan. They do participate in
8 understanding how these results are translated
9 into the design. They are part of the review
10 process from an assurance point of view.

11 We do make sure that we do keep the
12 arm's length relationship between design
13 authority responsibilities and design
14 assurance responsibilities. Our job is to
15 make sure that the process being followed is
16 in conformance with the standards that we've
17 expected and in conformance with the
18 expectations for ultimate public safety.

19 MEMBER BROWN: Thank you.

20 Dr. Shepherd, I've got a bunch of
21 questions here. I could talk to you forever,
22 as you know.

1 DR. SHEPHERD: Okay. Well, we've
2 got another hour.

3 (Laughter.)

4 MEMBER BROWN: The Chairman isn't
5 going to give me a full hour so let me run
6 through some things here if I can quickly. We
7 read a lot of your stuff. I know it's
8 probably dangerous quoting from somebody's
9 email without their permission, but I have an
10 email last November, November 2009, that I
11 would quote. There are a couple of things you
12 have at the end and I just wonder if you feel
13 the same way at this time.

14 DR. SHEPHERD: What day was that?

15 MEMBER BROWN: November 13, 2009.
16 You said, "The DNFSB [Defense Nuclear
17 Facilities Safety Board] comments span the
18 range from very minor to serious points with
19 some miscommunication thrown in for good
20 measure."

21 DR. SHEPHERD: Oh, boy.

22 MEMBER BROWN: "It is clear that

1 multiple reviewers were involved and some of
2 these comments are superficial while others go
3 to great depth and demonstrate understanding
4 of the issues. However, by focusing on so
5 much detail, I think the big picture may be
6 missed.

7 The DNFSB really needs to give some
8 priority and sense of importance so that the
9 main points can be addressed. From my
10 perspective the big issues are..." and you
11 list three. I would be interested in your
12 comments on these three big issues.

13 "...separating design and safety analysis.
14 This was the purpose of introducing QRA but
15 the issues are still entangled." Do you have
16 any --

17 DR. SHEPHERD: I would like to go a
18 little bit into the background here. This is
19 commenting on a document that had been
20 produced which had a set of questions and
21 comments about the approach at that time.

22 What I felt was oftentimes, and what

1 I see, and this is true not only of the
2 Defense Board but many other regulatory
3 boards, and it's perhaps just a fact of life,
4 but the comments span a large spectrum and
5 it's difficult to often get, I would say, a
6 response that really helps the organization.

7 I mean, the goal of all of this is
8 to help the organization to do its job in a
9 way that's going to comply with regulations,
10 going to make sure it's safe and it's being
11 done in a way and, in this case, safety means
12 it has to be done in an expedient fashion so
13 we don't leave the waste sitting in the
14 ground. That's been made clear.

15 My comments are really directed at
16 the fact that when the project organization
17 spends an inordinate amount of time responding
18 to each little detail and goes through each
19 one with almost equal importance, it really
20 then obscures what the main issues are. That
21 was really to the point of my comments here.

22 I felt they were really getting down

1 in the weeds and spending a lot of time
2 thinking about the details. I'm trying to
3 say, "Okay, guys. We need to step back a
4 little bit and say what's really the major
5 issues here." That's really the thrust of my
6 comments.

7 MEMBER BROWN: Thank you. The
8 second one was using test data and simulations
9 to validate the proposed method of treating
10 stress estimation from explosive loading.

11 DR. SHEPHERD: Right. So thinking
12 about these big issues and then just backing
13 up a little bit so I can clearly address each
14 one of these separating design and safety
15 analysis. This is a very important point that
16 hasn't really been touched on much here. This
17 may be more of my own opinion as a scientist
18 and an engineer than it reflects how the
19 project is approaching this.

20 I would like to point out that in
21 most projects of this type you have a design
22 which is driven by some fundamental

1 requirements of the job that you're trying to
2 do and then you have a set of safety analyses
3 that you do which are something that exist
4 separately to this.

5 This is something that has to be, I
6 think, clearly seen. You use the piping code
7 to do the design for your design basis. You
8 have a lot of safety analyses that you do that
9 consider all kinds of things. I always tells
10 folks when I get involved in these things all
11 things that are possible are not probable.

12 When you mix these things up and you
13 start to say, well, I'm going to do design,
14 for example, to resist as a standard case in
15 each piece of pipe, in each component, a
16 pressure reflected deflagration and detonation
17 transition, you've really put yourself in a
18 box that's extremely hard to get out of. I'm
19 not sure if that makes any sense at all.
20 That's what my comment one was about. You
21 should not get these two things confused.

22 Now, number two, using test data in

1 simulations to validate the proposed method of
2 treating stress estimation from explosive
3 loading. One of the key things that we have
4 to keep in mind here is that we have a complex
5 state of stress in the piping. Piping codes,
6 they are not like the 10 Commandments. All
7 right? The piping code is a very big
8 collection of prescriptions about how to do
9 things and it gives you many different ways to
10 do things.

11 One of the things that they tell you
12 is you really need to, as a responsible
13 engineer, figure out how you're going to treat
14 complex situations where you have stresses in
15 different directions -- in this case the
16 stresses are time dependent -- and how you are
17 going to combine those and then specify some
18 criteria that say whether or not you are going
19 to accept that level of combined stress. Now,
20 that's not something that we have any rules
21 about in the piping code.

22 One of the things that I think is

1 very important to do and that the project has
2 recognized and the project has been engaged in
3 for some time and isn't going to be completing
4 -- they've committed to doing that as part of
5 responding to the Independent Review Team's
6 remarks -- is developing methods and
7 validating for how you estimate the stresses
8 and combine those.

9 MEMBER BROWN: Thank you. I
10 appreciate the insight. That's what I'm
11 looking for. I'm always looking out. I like
12 to hear people looking back so I can validate
13 what I'm doing. One of the things which I
14 think you just explained but it's a quote out
15 of a 2009 Journal of Pressure Vessel
16 Technology that you wrote is that, "There is
17 no provision within the ASME boiler and
18 pressure vessel or piping codes for designing
19 pressure vessels or piping to withstand
20 gaseous detonations."

21 DR. SHEPHERD: That's correct. If
22 you'll look you'll see that there is a short

1 section with some recommendations about
2 deflagrations. We now have a code case that
3 is sort of a supplement to the code which
4 describes how you handle having solid
5 explosives inside of a containment vessel.
6 This is something that, in fact, was done for
7 the DOE for their testing facilities that they
8 have at the national laboratories.

9 There is not any specific
10 prescription about what you do when you have
11 a detonation inside of a pipe or a vessel and
12 so you have to rely on that part of the code
13 that says that you need to get smart,
14 qualified engineers and they need to use
15 accepted methods and analyze that and come up
16 with methods for then determining what the
17 stresses and strains are.

18 That's really what we've been about
19 here. I wrote that article a little while ago
20 and if I'm going to write an update in that,
21 I would include all of this new information we
22 have. In fact, we're working with the ASME --

1 both the boiler and pressure vessel part and
2 the piping part, to initiate a process, and
3 it's quite a lengthy process with the ASME.

4 It's a pretty bureaucratic
5 organization. Their engineers are very
6 deliberate and conservative -- in developing
7 a set of rules that would then allow for
8 basically translating everything that we've
9 learned here in this program plus additional
10 knowledge and then we would have a
11 prescription where people could go and look it
12 up and say, "Okay, what do I do now? I've got
13 a detonation. How should I estimate the
14 stresses and the strains?"

15 MEMBER BROWN: How long does it
16 typically take to get a code case through?

17 DR. SHEPHERD: The code case that
18 I'm familiar with is the one that was done
19 from impulsively loaded vessels and I think
20 that took about seven years.

21 MEMBER BROWN: So it's not
22 something done lightly.

1 DR. SHEPHERD: No.

2 MEMBER BROWN: Mr. Kasdorf talked
3 briefly about Hamaoka and Brunsbuttel and the
4 explosions that happened in those nuclear
5 plants. The information I have says that the
6 ductal pipe failures were estimated at
7 somewhere between 123 and 127 percent of their
8 normal dimensions but that was a different
9 type of material.

10 DR. SHEPHERD: There were two
11 different types of materials actually. I
12 think a couple really key differences between
13 those situations and the present one. In
14 Hamaoka it was carbon steel and high-strength
15 material and in Brunsbuttel it was stainless
16 steel. The stainless is more similar to what
17 we have here.

18 The other key thing is those systems
19 were operating at very high pressures to start
20 with and so if you look at the relative
21 loading, that is the pressure that was
22 produced, they believe, by the explosion

1 compared to the onset of plastic deformation,
2 those pressures were quite high in comparison
3 to the pressures that we're considering even
4 in the most extreme cases that we have, the
5 so-called pressure reflected detonation cases.

6 Those would still be much lower.

7 If, you fact, you look at the relative amounts
8 of deformation, they would be much, much
9 smaller here in the case of the WTP. I fact,
10 they are so small you would never even
11 consider fragmentation to be an issue in the
12 WTP in comparison to that.

13 MEMBER BROWN: I think I've read
14 that deflagrations you can expect possibly a
15 ten-fold increase in the pressure and a
16 detonation is 30-fold, something like that.

17 DR. SHEPHERD: It's good to think
18 about it in very definite terms. For the
19 hydrogen nitrous oxide system and we've been
20 using a system with about 30 percent hydrogen
21 as sort of the reference case. The pressure
22 increase that you get for a detonation would

1 be about 26 times and the pressure increase
2 for a deflagration might be on the order of 10
3 to 12 times.

4 MEMBER BROWN: It's 12 times the
5 original pressure?

6 DR. SHEPHERD: The original
7 pressure.

8 MEMBER BROWN: -- going back to the
9 nuclear power plants where they are operating
10 at 1,600 PSI multiplied by 26 and you get a
11 pretty significant --

12 DR. SHEPHERD: Exactly. Of course,
13 in that case that was a hazard people have
14 known about as long as we've been designing
15 nuclear power plants and they simply didn't
16 take care of the fact that they should have
17 had a high-point vent there and they could
18 have avoided that problem. That was the case
19 where standard mitigating method could have
20 been used to avoid that.

21 MEMBER BROWN: Thank you.

22 Mr. Ashley, we talked about what it

1 takes to get hydrogen deflagration or
2 detonation. You need the hydrogen, you need
3 the oxidizer, and you need the initiator.
4 What do you use as the probability of
5 initiation for hydrogen?

6 MR. ASHLEY: The probability of
7 ignition we use is 1. What we assume is if
8 the conditions exist, and this is through the
9 QRA, through the use of the QRA if the
10 conditions exist that could result in a
11 deflagration or detonation, we assume that the
12 ignition source is there.

13 MEMBER BROWN: Does that mean as
14 soon as you get to a detonable quantity or you
15 get the maximum detonable quantity and then
16 you --

17 MR. ASHLEY: Based on the event
18 under consideration we do not do like we did
19 in the ice condensers where we have hydrogen
20 igniters to make sure that we ignite before we
21 get there. We assume that the bubble
22 continues to accumulate so that we can be

1 evaluating the condition that would provide
2 the high severity of that specific event.

3 MEMBER BROWN: The HIRT team
4 questioned whether this was necessary. Is
5 that correct?

6 MR. ASHLEY: Well, this is a topic
7 of a lot of discussion. Could there be
8 through an expert elicitation process, poll a
9 bunch of experts together that could provide
10 a different -- rather than a probability of
11 one could we develop some other probability
12 distribution for ignition evaluating the
13 specific sources of ignition?

14 I think as Dr. Shepherd said the
15 condition in Brunsbuttel and in Japan were
16 very high pressure, high temperature.
17 Obviously we don't have that condition but
18 there was a recommendation that we might
19 evaluate something other than a probability of
20 ignition of one.

21 In terms of looking at specific
22 additional margin in our response to that

1 recommendation as we are considering an expert
2 elicitation but right now that is not a
3 priority for us. Our priority will be using
4 the design tool which assumes a probability of
5 ignition of one.

6 MEMBER BROWN: Thank you.

7 MR. RUSSO: Just for comparison, if
8 I may, our facility will run at about a
9 maximum of 140 F temperature, 70 to 80 psi.
10 The reactor, as you know, goes at about 500 to
11 600 F, 1200 to 1600 psi. I just wanted to
12 provide that for context and the discussion.

13 MEMBER BROWN: Thank you, Mr.
14 Russo.

15 The probability of ignition, Dr.
16 Shepherd, is that a reasonable assumption that
17 BNI is making? What was your opinion of the
18 HIRT recommendations on that subject?

19 DR. SHEPHERD: My opinion is that we
20 should reconsider the probability of ignition.
21 If you look at what drives the QRA which, by
22 the way, I believe is a very important tool

1 for understanding what you need to be
2 addressing in your safety analysis.

3 The probability of ignition in my
4 laboratory is zero except when I push the
5 button. If you have a piece of pipe that has
6 no active components in it, catalytic
7 materials, nothing is moving, it's just
8 sitting there, to me it's not credible to be
9 postulating that you have ignition taking
10 place.

11 When you say that the ignition
12 probability is one, you're doing something
13 that is more than just conservative. You're
14 basically throwing up your hands and saying,
15 "I'm not going to try to seriously address
16 this issue."

17 I think it's useful to look at what
18 other organizations have done. I have
19 encouraged the project all along to have a
20 look at what the practices are in various
21 other industries which have hazards. For
22 example, inside of aircraft fuel tanks looking

1 at what's been done at Sellafield.

2 We are now engaged in talking to
3 Sellafield about their practices that they
4 have there. They have, in fact, sponsored a
5 great deal of work on ignition by impact and
6 things of that nature. I think that whatever
7 you can do in regard to understanding better
8 and quantifying what the ignition sources are.

9 For example, I've never heard a
10 substantive discussion about what actually the
11 ignition sources would be other than just sort
12 of a very rough evaluation that, "Oh, well, we
13 might have some components that might generate
14 some kind of electrical spark or else there
15 might be some compressive ignition due to
16 motion of material."

17 Outside of that I don't believe
18 there has been any substantive evaluation of
19 that and I think there are substantial gains
20 that can be made.

21 CHAIRMAN WINOKUR: Okay. We are
22 going to take a question from Dr. Mansfield

1 and maybe one from Mr. Bader and we'll take a
2 very brief break. We need to do that. Then
3 we'll get back to Mr. Brown.

4 Outside of that I don't believe
5 there has been any substantive evaluation of
6 that and I think there are substantial gains
7 that can be made.

8 CHAIRMAN WINOKUR: Okay. We are
9 going to take a question from Dr. Mansfield
10 and maybe one from Mr. Bader and we'll take a
11 very brief break. We need to do that. Then
12 we'll get back to Mr. Brown.

13 MEMBER MANSFIELD: Just a short
14 intervention, Professor Shepherd. The gas
15 company has pipes under a fraction of an inch
16 of water pressure four feet underground, wet,
17 no sparks, no nothing. And yet, they always
18 assume a PLI of one. That's why they dig.
19 The same is true of the space shuttle main
20 engine testing facility.

21 Any leak of hydrogen at the West
22 Palm Beach test facility is considered to have

1 a PLI of one. Even though it's miles away
2 from -- not miles but a long way from anything
3 you and I would call emission facility. I
4 really don't think it's a good idea to
5 introduce PLIs of less than one in a facility
6 that you can't even see.

7 DR. SHEPHERD: I think what you have
8 to do is to look at the practices in a lot of
9 industries. For example, industries that
10 handle high-hazard flammable materials,
11 flammable dust, flammable gases, liquids, and
12 so on, there are standard electrical practices
13 for minimizing the sources of invert ignition
14 by any kind of accidental electrical
15 discharge.

16 There's an entire industry that is
17 devoted to this. There is an ATEC standard in
18 Europe. There are EL standards here in the
19 United States. As so one can make substantial
20 efforts to ensure that there are no ignition
21 sources present for a number of these types of
22 ignition sources.

1 Some are things that you can always
2 postulate and we are going to have difficulty
3 ever ruling out, for example, catalytic
4 materials inside of the piping systems,
5 adiabatic surges.

6 I believe it behooves the project if
7 we are going to turn over every rock and
8 understand what are indeed the threats. Then
9 we need to understand what is the realistic
10 probability of ignition and that's something
11 that I think ought to be included in the QRA.

12 CHAIRMAN WINOKUR: Mr. Bader.

13 MEMBER BADER: Mr. Ashley, all this
14 discussion with Dr. Shepherd and yourself just
15 continues to drive me in the direction of
16 asking you a similar question to what I asked
17 Dr. Shepherd. When you look at all these
18 uncertainties, and I can reenumerate them but
19 you've heard them before, and you've added a
20 few more, doesn't this drive you in the
21 direction of needing additional prudent levels
22 of conservatism?

1 MR. ASHLEY: We believe that we do
2 have prudent levels of conservatism.
3 Certainly it's good to step back from this and
4 understand really the two sides to the
5 equation, the demand side and the capacity
6 side.

7 The demand side is really governed
8 by what we're doing through the quantitative
9 risk analysis. What is the accumulation of
10 hydrogen, what is the geometry of that
11 accumulation of hydrogen, and what the
12 resulting potential events could be. Even
13 embedded in that methodology is conservatism.

14 The capacity side is very
15 deterministic and conservative. If you look
16 at the methodologies employed in combinations
17 of stresses, look at the methodologies
18 employed in the analysis to predict responses,
19 and then look at the methodologies that are
20 employed in determination of the material
21 properties and the levels of stresses that are
22 allowed. That is very deterministic and

1 conservative.

2 We believe that though there are
3 those uncertainties, and we acknowledge those
4 uncertainties, and through the QRA we actually
5 can evaluate the sensitivity to those
6 uncertainties, we believe that what we have is
7 what we termed in commercial nuclear high
8 confidence, low probability of failure which
9 is assuring that we maintain, even in these
10 unlikely events, probability of ignition of
11 one and even under these unlikely events we
12 maintain the pressure boundary of the piping.

13 MEMBER BADER: Let me go to one
14 other thing and I appreciated this comment
15 that Dr. Shepherd made. He talked about
16 getting lost in the weeds looking at all the
17 small details. Wouldn't adding back even more
18 conservatism allow you to get much less
19 complex situation in determining the risk from
20 hydrogen detonations --

21 MR. ASHLEY: Actually --

22 MEMBER BADER: -- which is going

1 back to where we were before.

2 MR. ASHLEY: Well, I think it's
3 important when you talk about where we were
4 before in the approval of the criteria in
5 2006.

6 There were basic assumptions that,
7 in fact, we provided significantly more rigor
8 that we believe is important in looking at
9 potential, the possibility of multiple events
10 and what affect those multiple events have on
11 the systems in looking at components of stress
12 that originally prior to doing all of the
13 investigation testing and analysis that we may
14 not have considered.

15 You can look at it and say there is
16 a lot of complexity in the journey, a lot of
17 moving parts. The intent is we have criteria
18 now that is easily understood. It's not
19 implemented by everyone. These are
20 specialists that are implementing this
21 criteria all the way from the organizations
22 and the personnel that provide input to the

1 QRA; engineering, operations, and safety.

2 Even the analysts, back from the
3 commercial nuclear days, you didn't give
4 transient analysis of piping systems to any
5 engineer. You didn't give class 1 analysis of
6 piping systems to any engineer. Those were
7 specialists. This criteria will be
8 implemented by specialists. It's important.

9 MEMBER BADER: The last question
10 before we break to Ms. Busche. Staying on
11 this course to me means that there will have
12 to be assumptions that are fairly complex,
13 protected in the safety basis.

14 MS. BUSCHE: Correct. 3009 Appendix
15 A would drive us there when I analyze this
16 design tool like any other design tool.

17 MEMBER BADER: And that's going to
18 be a more complex situation in the operation?

19 MS. BUSCHE: I don't think I can
20 determine that yet but we will have to
21 maintain it and establish programs that are
22 different than what we would traditionally

1 have today.

2 MEMBER BADER: If you see an
3 occurrence in the plant during operation,
4 wouldn't you have to then go back and
5 challenge?

6 MS. BUSCHE: Yes.

7 MEMBER BADER: Thank you.

8 MR. ASHLEY: Mr. Bader, I do need to
9 add to that. If you look at all of the
10 parameters that are necessary or that are
11 important in the PRA [Probabilistic Risk
12 Analysis], many of these parameters are
13 already protected. Maximum temperatures of
14 systems, the hydrogen generation rates. Those
15 are protected already.

16 If you look at many of the
17 assumptions in the probability distributions
18 those are protected by existing safety
19 management programs. There are safety
20 management programs that will be necessary for
21 the plant.

22 We will need to review, and nuclear

1 safety will need to review, are there any
2 additional assumptions that require
3 protection. I think the thought that the QRA
4 is creating a whole new set of protected
5 assumptions, that's not true. That's not
6 factual because a lot of the inputs are
7 already protected design basis assumptions.

8 CHAIRMAN WINOKUR: All right. I
9 think we're going to need to take a short
10 break right now. It's only going to be two or
11 three minutes and then we will pick up. Okay?

12 (Whereupon, at 10:26 a.m. the above-
13 entitled matter went off the record and
14 resumed at 10:30 a.m.)

15 CHAIRMAN WINOKUR: All right, we're
16 going to reconvene. Please, I would like quiet
17 in the room.

18 Mr. Brown, you can continue your
19 questioning.

20 MEMBER BROWN: Thank you, Mr.
21 Chairman.

22 Let's see. Dr. Shepherd, can you --

1 we had hoped Dr. Mattson could be here but he
2 was unable to be here for significant personal
3 reasons so I guess I have you to talk to about
4 the HIRT team. Can you describe what your
5 role was with the HIRT team or as an adjunct
6 to the HIRT team?

7 DR. SHEPHERD: I wasn't a member of
8 the team. I briefed them on my activities.
9 They came to Cal Tech and I gave them
10 presentations on our work. We had two test
11 programs that were sponsored by the DOE in
12 2008, 2009, and 2010 so I talked about that
13 work.

14 I gave them the results of that
15 work, access to the web pages where the data
16 is, access to the reports. Then I also
17 engaged in discussions primarily with two of
18 the review team members that were looking at
19 gas phenomenology, that was Chickarelli and
20 Lee.

21 I also engaged in some discussions
22 with the group that was looking at structural

1 response. I reviewed portions of the documents
2 and provide comments to them. That was the
3 extent of my involvement.

4 MEMBER BROWN: So you were brought
5 in as an adviser. You haven't really been
6 following the implementation of their findings
7 or --

8 DR. SHEPHERD: Right. I should add
9 to that no, I was involved in the discussion
10 of the plan that was put together by the
11 project to respond to the findings and so I
12 have made comments on several of the areas and
13 there were several of those areas where I felt
14 that there should be responses that folded in
15 some of my concerns that I have brought up in
16 reviewing some of the other documentation. My
17 comments have been noted and incorporated into
18 that response plan.

19 CHAIRMAN WINOKUR: Okay, Mr. Brown.
20 I hope we have one or two more and we might
21 need to move on, please.

22 MEMBER BROWN: Okay. Just two more

1 questions.

2 CHAIRMAN WINOKUR: Great.

3 MEMBER BROWN: Maybe three. The
4 HIRT team had recommended that BNI establish
5 plastic collapse design margins by testing
6 representative piping and components to
7 failure or by analytical calculations. Do you
8 have any comments on that recommendation?

9 DR. SHEPHERD: I think it's nuts.

10 MEMBER BROWN: Excuse me?

11 DR. SHEPHERD: I don't think it's
12 rational to propose doing that. It doesn't
13 make any sense. I mean, the kinds of loads
14 that we're talking about to get to plastic
15 collapse are so extraordinary and outside of
16 anything that we would imagine that we have
17 either tested or postulated that I don't know
18 what value that would add to the program.

19 MEMBER BROWN: Thank you. The
20 question for you, and then Mr. Ashley,
21 basically the same question. What further
22 tests or analysis do you consider important to

1 the subject of hydrogen explosions in piping?

2 DR. SHEPHERD: Let's be clear.

3 We're talking about HPAV here.

4 MEMBER BROWN: HPAV.

5 DR. SHEPHERD: Yes. I think one of
6 the most important things we can do at this
7 point is to complete the work that Bechtel has
8 said that they are going to do, the project is
9 going to do in regard to fleshing out the
10 design rules and going through an example of
11 that and making sure we have a very clear
12 statement about how the stresses are going to
13 be combined and have an end-to-end calculation
14 for a model system that clearly explains to
15 the designers about how to apply what has
16 evolved into a fairly complex set of design
17 rules that they will need to use to evaluate
18 situations where you have detonations in
19 piping.

20 I think that is the most important
21 thing to do at this point is to make sure
22 that's really very clearly all set out and

1 worked through. In fact, this is a concern
2 that I believe they have committed to
3 responding to and I think that is the most
4 important thing.

5 MEMBER BROWN: Thank you, Dr.
6 Shepherd.

7 Mr. Ashley, would you care to
8 comment on that?

9 MR. ASHLEY: The remaining testing
10 that we must do is for component
11 qualification. We're in the process of
12 developing the test plans and acceptance
13 criteria for qualification testing of
14 components. Once again, though, that's very
15 different than the testing that has been done
16 over the past five years. This is, I would
17 say, a different qualification for a different
18 load, a different event, but it is similar to
19 seismic qualification of components or
20 environmental qualifications.

21 As we purchase a piece of equipment
22 the requirement for testing whatever the

1 safety function is for that component will be
2 part of that procurement.

3 MEMBER BROWN: Thank you, Mr.
4 Ashley.

5 Mr. Chairman, those are all my
6 questions.

7 CHAIRMAN WINOKUR: Thank you, Mr.
8 Brown.

9 Dr. Mansfield.

10 MEMBER MANSFIELD: First, I would
11 like to go back to the last question that Ms.
12 Roberson asked about who measures what,
13 hydrogen, nitrogen, and where. It was unclear
14 because, Mr. Ashley, you said we. I'm sure
15 that was the corporate institutional we. What
16 I want to ask about is when you have to know
17 the hydrogen generation rate and the N2O
18 generation rate -- the N2 generation rate in
19 pipe, who collects that data, from what sample
20 and where?

21 MR. ASHLEY: Okay. There will be a
22 collection of that data. It is a requirement

1 of the waste acceptance criteria so before a
2 feed is set, it's sent to the WTP. That
3 certification parameter will be collected.

4 MEMBER MANSFIELD: By the operators
5 of the waste treatment plant?

6 MR. ASHLEY: I'm not -- it is in the
7 waste acceptance criteria. In terms of
8 specifically which organization, obviously at
9 the time we're operating the operator will
10 have to receive that certification of that
11 sample before that feed is transmitted to the
12 WTP. The tank farm.

13 MEMBER MANSFIELD: The tank farm.
14 Okay. Is the hydrogen generation rate
15 measured or is it a mass-weighted calculation
16 based on the Hu result from a bunch of
17 different batches that have been blended
18 together.

19 MR. ASHLEY: It's measured.

20 MEMBER MANSFIELD: Measured. The
21 same is true with the N2 and N2O?

22 MR. ASHLEY: There are a set of

1 gases and I don't have the ICD in front of me.
2 There are a set of gases, hazardous gases that
3 will have to be measured.

4 MEMBER MANSFIELD: Are those done
5 in your laboratory facility at the WTP plant
6 or a new facility or where?

7 MR. ASHLEY: I would have to defer
8 that to --

9 MR. SAIN: 222S.

10 MEMBER MANSFIELD: Oh, 222S. Okay.
11 Fine. Good.

12 The next few questions I have are
13 based on DOE's answers to the Board's written
14 questions from some time ago most of which are
15 for you, Mr. Ashley, but there is a sprinkling
16 for others. You have certainly heard from the
17 Chairman that the operability of the plant is
18 a safety issue. If you break the plant,
19 safety suffers.

20 MR. ASHLEY: Yes.

21 MEMBER MANSFIELD: So, you are
22 going to have to forgive us if we ask

1 questions and expect you to have controls like
2 on hydrogen of the most conservative type
3 because of the fact of what might be a simple
4 industrial problem is liable to be months or
5 more of exposure to the tank waste. We are
6 not letting up on that.

7 Mr. Knutson, when ORP [Office of
8 River Protection] approved BNI's request to
9 modify the design strategy for control of
10 hydrogen in pipes you established multiple
11 criteria for the magnitude of plastic strain,
12 number of strain events, and things like that,
13 to protect the primary boundary.

14 It's getting very complex and it's
15 getting more so. You need now to watch over
16 30 parameters to make sure you have accurate
17 values or accurate distributions for them as
18 opposed to five parameters last year. Is this
19 getting too complex for the owner of the plant
20 to manage?

21 MR. KNUTSON: The assessment report
22 that I mentioned in my opening remarks

1 evaluated one of the areas which was how have
2 we established expectations for safe
3 performance and the ability to manage our
4 ability, the Department of Energy's ability,
5 to manage the evolution of responsibilities as
6 we move forward.

7 The complexity of the controls and
8 the assessments associated with those controls
9 inside the Department of Energy has not
10 increased. The assessment processes that are
11 used to ensure that those controls are
12 monitored and evaluated has not become more
13 complex.

14 The relationship between WTP as a
15 project and the Office of River Protection as
16 a site office and authorization basis has got
17 to continue to mature so that as this evolves
18 we can continue to keep a pace with the
19 evolution of the project.

20 All of that is an expected outcome
21 of a project of this scale, a project of this
22 size, moving from a design and construction

1 activity to a commissioning and operations
2 activity. Now, that is a standard and normal
3 expectation associated with any major project
4 evolving towards commissioning, especially one
5 that's a non-reactor nuclear facility in the
6 Department of Energy.

7 MEMBER MANSFIELD: But this
8 complexity is going to continue into operation
9 of the plant. You're going to have to
10 continually review, it seems to me, the
11 contractor's performance on protecting the
12 safety base of many more variables than you're
13 used to.

14 MR. KNUTSON: The normal practice,
15 normal process of our mission-driven site
16 office and Department of Energy activity is
17 exactly that. We must stay a pace with the
18 way the plant is evolving and we must remain
19 cognizant of the way the safety basis is being
20 implemented.

21 MEMBER MANSFIELD: I would have
22 asked this question of Dr. Mattson, and I will

1 eventually, but I'll ask it of you now in his
2 absence. The output of a route-by-route
3 calculation, QRA calculation, as I understand
4 it in the ideal situation, probability density
5 function for the strain in a pipe that can be
6 compared with the ultimate strain to tell you
7 whether you are close to failure or not.

8 Correct?

9 MR. ASHLEY: I think as I said
10 before, Dr. Mansfield, the QRA provides the
11 demand side of the equation, not looking at
12 the capacity side of the equation.

13 MEMBER MANSFIELD: You
14 misunderstand me. If you want, you have a QRA
15 for the demand side required to cause a
16 certain strain that you have decided is either
17 code limit or a limit established by the
18 consensus of people looking at plastic
19 deformation. I mean, there is a probability
20 density function for something in this
21 problem. That's the only thing I can see
22 comes out of the QRA.

1 MR. ASHLEY: What comes out of the
2 QRA really is the severity of the event and
3 the frequency of the event. Then what we have
4 --

5 MEMBER MANSFIELD: That's a
6 probability density function.

7 MR. ASHLEY: That's correct. Then
8 what we have to do with that is take those
9 peak pressures, the severity of the event, and
10 the number of times that event could occur and
11 we evaluate that through the response
12 predictions, the piping response predictions
13 to compare that against our acceptable
14 strains.

15 MEMBER MANSFIELD: Okay. You are
16 trying to do this without, of course, code
17 guidance along the lines that we mentioned
18 just a few minutes ago. It seems to me that
19 requires a burden of independent review on
20 parameters and methods and probability density
21 functions, gas pocket logic and things like
22 that, that would normally not be the case.

1 There is no cookbook here. Somebody
2 has got to look at your assumptions or
3 calculations or determinations of what the
4 probability density functions of various
5 parameters in the expressions used through the
6 gas pocket logic to the EPC [Engineering,
7 Procurement and Construction], etc.

8 Unknown parameters that are not
9 allutory parameters -- do you agree they are
10 best treated as random variables as NUREG-1855
11 [Nuclear Regulatory Commission Regulation]
12 recommends? There being no guidance from DOE
13 on whether or not you should do this, do you
14 believe that you have to -- that it's
15 necessary to treat unknown variables as random
16 variables for the purpose of doing these
17 calculations?

18 MR. ASHLEY: Actually in one of the
19 recommendations that came out of the HPAV
20 Independent Review Team as we looked at the
21 inputs to the PRA is that many of the inputs,
22 as you remember, Dr. Mansfield, were point

1 values.

2 I think when you were here in a
3 smaller briefing I believe in March and we
4 provided you a table of what the basis for the
5 input values, one of the recommendations that
6 came out of the Independent Review Team is
7 obviously looking at those point values and
8 many of those should be input as probability
9 distribution functions. Right now we have 73
10 existing parameters and 35 of those are being
11 converted to probability density functions.

12 As you mentioned, one important part
13 of implementation of a PRA or a QRA is peer
14 review. And as we've responded to the HPAV
15 Independent Review Team findings are when the
16 QRA when we have addressed the findings and
17 those recommendations that we will address, we
18 will submit the QRA to independent peer
19 review, a peer review team of three.

20 One of the peer reviewers that
21 actually DOE -- when DOE did their peer review
22 out of Brookhaven one of those reviewers will

1 be there. One of the members that was the PRA
2 expert that was on the HPAV Independent Review
3 Team and then there will be a third expert
4 that will be called --

5 MEMBER MANSFIELD: By route?

6 MR. ASHLEY: -- that will be called
7 in to review the PRA methodology.

8 MEMBER MANSFIELD: Methodology.

9 MR. ASHLEY: We will not have
10 actually run the PRA until we get through the
11 completion of the implementation of the
12 findings, a resolution of the findings,
13 complete the V&V [Verified and Validated] of
14 the tool in accordance with the NQA1
15 requirements [Nuclear Quality Assurance] and
16 the 414-1C requirements. It will then be
17 ready for implementation, i.e., route by route
18 taking the methodology and applying that
19 methodology to the specific routes.

20 MEMBER MANSFIELD: And that would
21 be the case for all situations where
22 parameters can't be determined precisely and

1 there is a good argument that they should be
2 distributed.

3 MR. ASHLEY: That's correct. All of
4 those probability distributions will be
5 documented in terms of what is the basis of
6 the selection of that probability
7 distribution.

8 MEMBER MANSFIELD: And that's a
9 promise?

10 MR. ASHLEY: That's correct.

11 MEMBER MANSFIELD: Ms. Busche,
12 you're the only nuclear safety expert
13 testifying today and you're a good one or
14 otherwise we wouldn't have asked you here.
15 Are these QRA results far enough along where
16 you can conceive of how they can be used and
17 protected in the safety basis for the plant?

18 MS. BUSCHE: I am comfortable with
19 the construct of the tool, how it's been put
20 together with the caveat of the changes that
21 are being made. There are two primary input
22 tables that I would initially focus on or we

1 would initially focus on in our integrated
2 safety reviews and those would be your basic
3 event parameter tables and your event duration
4 parameter tables.

5 We would need to make sure if you're
6 using a frequency distribution or probability
7 density, whatever terminology you are going to
8 use, that we are consistent in the unmitigated
9 accident analysis and what this tool would
10 provide. Then we would make some
11 determination on those inputs and assumptions
12 and determine if they needed to be protected
13 by TSRs [Technical Safety Requirement].

14 Many, as mentioned before, are being
15 -- that parameter will have already been
16 selected because of another potential upset in
17 the plant. To understand the inputs and
18 tanks, it's not mature enough along that I can
19 make those determinations.

20 MEMBER MANSFIELD: In a nuclear
21 power plant or in other chemical plants
22 initiating events like that that can't be

1 controlled, for instance, loss of offsite
2 power and duration of offsite power, are
3 mitigated by having enough electric power to
4 protect the plant.

5 I raised questions yesterday about
6 whether that is the case and whether it's
7 wise. I just raised them again. I've never
8 seen a plant this important and this expensive
9 that wouldn't have -- was at the whim of
10 nature and the utility company to protect it
11 from further damage. Would you care to
12 comment on that?

13 MR. ASHLEY: Yes. Obviously all of
14 those would meet the requirements important to
15 safety equipment that must be maintained from
16 a nuclear standpoint in the loss of offsite
17 power. Additional loads on a diesel are
18 obviously evaluated as a risk decision.

19 That risk, as we've talked about,
20 one of the important features of that is if we
21 did not have those components available what
22 would be the potential impact on the operation

1 of the plant. I think you recognize that
2 those components that are not important to
3 safety you can't put everything on your
4 emergency diesels.

5 In commercial nuclear days one of
6 the last things we did is what are the
7 essential loads because we have too many loads
8 on our diesels. You can't have lighting on
9 your diesels. You can't have some of the
10 components because you are limited in terms of
11 diesel loads.

12 One of the beauties of the QRA,
13 though, is allowing us to make those types of
14 decisions, providing that information that
15 really allows us to evaluate the risk and make
16 those decisions. Good examples are we are
17 using very conservative assumptions in terms
18 of loss of offsite power.

19 One of the parameters this facility
20 has used is loss of off-site power for a
21 thousand hours. It's a long time. Forty days
22 with no power. There's a lot of action that

1 could be taken during a 40-day period but
2 there are conservative assumptions in terms of
3 what those event probabilities are, what the
4 distribution of those events are. Those are
5 all essential elements to a PRA.

6 MEMBER MANSFIELD: But, for
7 instance, on a thousand hour loss of offsite
8 power it's probably due to some event that
9 will take all the bridges down. If you were
10 thinking of trucking in a diesel, you know,
11 you don't have many options. Once you've
12 built a plant, I think you have to consider
13 that the options are totally limited.

14 Another argument for having
15 everything reviewed, I'm reminded of the
16 complex codes used for fire protection
17 calculations. They are not only reviewed
18 externally, they are reviewed on a national
19 basis. There are whole code cases on how you
20 calculate how fires spread in a building.

21 Your models for hydrogen generation
22 and detonation deserve a level of review

1 that's equally strong. Do you agree to that?

2 MR. ASHLEY: We believe we have
3 subjected these models to very extensive
4 independent review. This is the methodology
5 even from the beginning with world renowned
6 experts in the specific areas and specific
7 disciplines including Dr. Shepherd's ongoing
8 involvement and the 12 members of the HPAV
9 Independent Review Team.

10 This has also gotten a lot of
11 attention. Some of the documentation has been
12 provided. I believe, Dr. Shepherd, that the
13 7-11 document has been provided to the Nuclear
14 Regulatory Commission.

15 DR. SHEPHERD: I can comment on this
16 a little bit. I was recently involved in
17 review of advanced reactor design for
18 licensing and they were attempting to do some
19 evaluation of a situation where they had
20 detonation in some piping and I got permission
21 to transmit this document, this so-called 07-
22 11 document, and I felt that would really

1 substantially help the NRC and the industry
2 out in doing that.

3 I agree with you that in the best of
4 all worlds we would have a broad exposure and
5 review and participation from many
6 communities. This is a very specialized
7 business. There's not really that many people
8 who are working on the subject of detonations
9 inside of pipes.

10 MEMBER MANSFIELD: There's not many
11 people that are working with such consequences
12 either.

13 DR. SHEPHERD: Well, that's right.
14 It's a very small community. You could ask
15 the National Academy of Sciences to be
16 involved and so on but the difficulty is
17 really in getting enough folks together and
18 having a critical mass. Loss of life due to
19 fire, I would point out, is something that is
20 of much more substantial and broader interest
21 to the society.

22 MEMBER MANSFIELD: But that is

1 until there is a radiation incident.

2 DR. SHEPHERD: I understand.

3 MEMBER MANSFIELD: On the question
4 of unsteady expansion behind the detonation
5 front, you are proposing to examine whether
6 you can model this with a double exponential.
7 The parameters in a double exponential would
8 be what, would they be functions of time?

9 DR. SHEPHERD: What you're
10 addressing is the empirical description that
11 is being used for deflagration to detonation
12 transition. I just want to make a distinction
13 here, Dr. Mansfield, to be clear. When we
14 treat propagating detonation waves we have a
15 very sound basis to do this, the so-called
16 Taylor's Altovich Model, and this comes from
17 solving some gastronomic equations. That is
18 something we have a very clear grasp on.

19 What is much more difficult to do is
20 when we have transition from a deflagration to
21 detonation we have a very transient event.
22 The pressures that we get out of that are

1 something that are different each time we do
2 that experiment. What we strove to do in
3 constructing a model pressure signal was to
4 construct something that would bound the
5 strains that were measured by calculated
6 strains using that load input.

7 Those exponential functions
8 currently the version of that that has been
9 implemented today uses constants for those --
10 time constants -- but it has been proposed,
11 particularly by the independent review team,
12 that correlation be reexamined and potentially
13 that those constants could be calculated so
14 that they depend on other variables.

15 For example, the size of the gas
16 pocket. They would not necessarily be time
17 dependent. The time dependence would all be
18 in the exponentials but the time constant
19 itself would be depend upon the scale of the
20 system.

21 I would point out, though, that on
22 the other hand all that would do is provide a

1 little bit more of a connection to the physics
2 of the problem. I don't believe that the
3 Independent Review Team felt that it would
4 really necessarily change the answer in terms
5 of what the peak strains were.

6 MEMBER MANSFIELD: Wouldn't it
7 change the impulse?

8 DR. SHEPHERD: This is an
9 interesting question. What happens in these
10 problems is it's a kind of a mixed load. Both
11 the peak pressure and the duration are
12 important. Quite frankly it's an ad hoc
13 correlation.

14 There's a lot not to like about it
15 but what you really want to make sure that you
16 do is that you bounded all of the data that
17 you have and that's how it was selected.
18 There's a lot of changes that can be made to
19 that. There is not a unique way to prescribe
20 it because it's not based on a detailed
21 physical description.

22 MEMBER MANSFIELD: On the issue of

1 bends in elbows and asymmetry factors, the
2 variables used to calculate asymmetry factors,
3 or estimate asymmetry factors, are those going
4 to be considered distributed because they are
5 epistemically unknown or uncertain?

6 MR. ASHLEY: The asymmetry factor I
7 can let Dr. Shepherd weigh in on that but
8 asymmetry factors actually were developed from
9 the correlations with the test.

10 MEMBER MANSFIELD: Okay. So those
11 test results.

12 DR. SHEPHERD: Both test results and
13 there are some very nice pencil and paper
14 analysis. I'm patting myself on the back
15 here. I wrote a whole report about it. It's
16 basically the kind of analysis that you do
17 just when you have a garden hose and you turn
18 it on and it starts flopping around.

19 It's just momentum conservation.
20 There's nothing all that fancy about it. That
21 is pretty sound. I would say it's more than
22 pretty sound. I would say it's one of the

1 significant accomplishments we have is that we
2 have a good method for calculating the forces
3 on detonation.

4 MEMBER MANSFIELD: So you think
5 those are quite precise?

6 DR. SHEPHERD: Yes. They are
7 precise but underlying that is you have to say
8 I have a detonation in this bend. That's
9 what's imprecise.

10 DR. SHEPHERD: Of course but we know
11 that's where all the --

12 MEMBER MANSFIELD: Right.

13 DR. SHEPHERD: There is no
14 imprecision once you tell me I've got a
15 detonation in the mixture with 45 percent
16 hydrogen and nitrous oxide at 112 kPa and 50
17 degree C I can tell you what that force is
18 within 10 percent.

19 MEMBER MANSFIELD: Mr. Ashley, in
20 your operation frequency analysis
21 calculations, I'm referring to the so-called
22 008 report, you use failure data above the

1 means modes or error factors from Savannah
2 River, from EG&G [Edgerton, Germeshausen, and
3 Grier, Inc.], and apparently Bechtel has its
4 own reliability, availability,
5 maintainability, inspectability database.

6 What is the pedigree of those? Do
7 they include or are they consistent with a
8 very large database for industrial equipment
9 that is maintained by NRC and NRC contractors
10 and IEEE [Institute of Electrical and
11 Electronics Engineers] gold book and things of
12 that nature?

13 MR. ASHLEY: Yes. As we talked
14 about a little bit earlier, Dr. Mansfield, in
15 terms of the justification for all of the
16 probability distributions that are being used
17 in the QRA, in the quantitative risk analysis,
18 there is a basis, the basis being a
19 comparative basis back to substantiated
20 information. If there is information that we
21 need to use because, as you know, some of our
22 equipment is unique, then there will be a

1 basis provided that substantiates those
2 distributions.

3 MEMBER MANSFIELD: Most of those
4 distributions show up in the databases as a
5 central value and error factors on each side.

6 MR. ASHLEY: Actually, one of the
7 recommendations that came out of the HPAV IRT
8 is a number of these distributions were
9 modeled as triangular distributions. That
10 presumes that you know a maximum and that you
11 know a minimum.

12 MEMBER MANSFIELD: No. That's the
13 precisely the answer I didn't want unless you
14 prove to me that there is no possibility of an
15 extreme event past where that triangle ends.

16 MR. ASHLEY: You didn't let me
17 finish. Those are being changed.

18 MEMBER MANSFIELD: Okay.

19 MR. ASHLEY: Because we know that
20 there is no finite maximum and minimum for
21 many of those distributions. The original
22 drafts of those distributions did indicate

1 triangular distributions. As I said, that
2 would presume that you know the maximum and
3 the minimum. In a true probability
4 distribution you know that you don't.

5 MEMBER MANSFIELD: If the data
6 shows -- if the handbook data or the databases
7 show central values plus error factors in
8 either direction, that suggests to me that
9 they came from log normal distributions
10 because that's exactly the way to specify the
11 standard deviations of a log normal
12 distribution. Do you think that -- do you
13 share the widespread prejudice that log normal
14 distributions are in some sense natural for
15 these complex phenomena that involve multiple
16 parameters?

17 MR. ASHLEY: I can't say that I
18 share that but, as I said, we will develop the
19 distributions for those specific functions and
20 those will be provided both for the peer
21 review as well as will be open to anyone's
22 review.

1 MEMBER MANSFIELD: You mentioned in
2 response to our question on code cases for
3 extending the BDOT 31 code to explosive events
4 that it's not applicable. Is that really
5 precise? The 300-C3 and 300-C5 are applicable
6 but they don't solve your problem completely.
7 Appendix P on deflagration loads, those are
8 certainly applicable. Aren't they?

9 MR. ASHLEY: When we look at a
10 submittal of a code case, obviously you have
11 to step back and ask yourself the question
12 what are you asking the code to rule on. As
13 I think Dr. Shepherd indicated, B31 has
14 established a subcommittee that is looking at
15 development of a standard which is this is
16 very much not taking existing code and asking
17 the code for a ruling of -- your methodology
18 for adapting the existing code.

19 You're not also asking for a code
20 interpretation. This, in fact, is as the code
21 prescribes, the engineers identified that
22 there is a phenomena. There are loads. There

1 is a condition not addressed by the code. The
2 competent engineer as supported by the
3 necessary expertise is developing that
4 methodology within the framework of the code.

5 MEMBER MANSFIELD: After all, the
6 static code was developed to -- there's some
7 physics behind that. I mean, fiber bending
8 strength and things like that. The approach
9 to the Dinex vessel used a lot of physics
10 about metals and things like that and
11 presumably can serve as the basis for trying
12 to extend that.

13 CHAIRMAN WINOKUR: Ms. Roberson has
14 a question.

15 VICE CHAIR ROBERSON: Connecting to
16 Mr. Mansfield's question. In response to
17 question 5C, I'm going to ask you, Mr. Ashley,
18 because you are identified as a primary author
19 of the response, the question was identified,
20 "Other defense nuclear facilities that allow
21 gaseous deflagration, detonations in process
22 piping..."

1 In your response you sited the
2 Defense Waste Processing Facility in H-Canyons
3 at Savannah River as having been evaluated to
4 allow for gaseous deflagration, detonations,
5 and process piping. Then you say the safety
6 design strategies for these facilities haven't
7 been provided as part of the response.

8 I guess the question is we're asking
9 for the reference for those. We understand
10 that they were reviewed to determine the
11 probability and the capability of the as-built
12 facilities to handle those following the two
13 international events but we are not aware that
14 was a goal in the design strategy so we are
15 asking for references if you have any. That's
16 one.

17 MR. ASHLEY: Yes. I think I would -
18 - you know, those are other facilities, other
19 DOE facilities that I would refer to DOE to be
20 able to provide those. As the contractor, I
21 wouldn't be the one to provide those but I
22 would --

1 VICE CHAIR ROBERSON: Okay. That's
2 one. Then the second question on the same
3 response in regard to the Dinex facility which
4 your response is clearly the Board does have
5 a lot of knowledge about this. We understand
6 for that facility they also developed and
7 submitted a code case and they were very
8 discrete on specific actions that resulted.
9 You say you gained insights from that. What
10 insights did you gain?

11 MR. ASHLEY: That's correct.
12 Obviously one of the experts that has
13 supported us was working at Los Alamos at the
14 time and was actually one of the authors of
15 the code case. He has been on our team since
16 the beginning so obviously the insights that
17 were gained through development of that code
18 case, that individual was able to bring to
19 bear to development of our criteria. That
20 individual is Ed Rodriguez.

21 VICE CHAIR ROBERSON: Okay.

22 CHAIRMAN WINOKUR: Dr. Mansfield.

1 MEMBER MANSFIELD: I'm sorry to
2 take so much time but I'm the guy who was
3 assigned this stuff so I've got to do it. On
4 the 021 report, the implementation of closure
5 plan for the HIRT report, you mentioned that
6 the inline component test plan is not
7 completed and you've only done limited
8 testing. Do you have a time line for that
9 when you're going to have an inline component
10 test plan?

11 MR. ASHLEY: Yes. We expect to have
12 that test plan and test acceptance criteria,
13 I believe, by the end of November, that time
14 frame. We're working that obviously to
15 support the project schedule for procurement.
16 The nature of our procurement processes are
17 long. We obviously will have to source the
18 qualified lab to be able to do that testing.

19 There are a number of labs that are
20 qualified to do that type of testing, not just
21 going back to the one laboratory that we had
22 used previously in our testing. We are moving

1 on the schedule necessary.

2 I think it is important to point out
3 though, that we did do demonstration testing,
4 not qualification testing when we were doing
5 the large scale testing down at Southwest. We
6 believe that provides us the confidence that
7 we will be able to procure equipment that will
8 meet our requirements.

9 MEMBER MANSFIELD: I'm sorry to
10 have passed you up, Secretary Triay. Does
11 anything you heard here this morning
12 communicate to you that it's pretty urgent
13 that we get a risk policy with some direction
14 to contractors on how to handle these issues?4

15 DR. TRIAY: I believe that is why I
16 offered Dr. Krahn to come up yesterday. Let
17 me just summarize perhaps in a little bit more
18 detail the work that he is doing as the head
19 of the Technical Authority Board.

20 The Environmental Management Program
21 worked with the Board to promulgate some of
22 the basic principles of Standard 1189 through

1 the Technical Authority Board ahead of the
2 formal policy of the Department because we had
3 facilities that were in the design and were
4 being built for tank waste across the complex.

5 I believe the Technical Authority
6 Board can serve the same function for the
7 waste treatment plant, the policy that I
8 promulgated at the Environmental Management
9 Program level through the Technical Authority
10 Board.

11 MEMBER MANSFIELD: It seems to me
12 you're the one most affected by the incomplete
13 art of probabilistic safety assessment at DOE.
14 Frankly, this needs a champion. You've heard
15 today that many of the questions that we've
16 had would have disappeared, would not have
17 been here, if certain NUREGs had been accepted
18 by the project at the start.

19 I mentioned 1855 which says that all
20 epistemic variables should be considered
21 candidates for being random variables. That's
22 a very good thing to do and is widely done.

1 It was not done here until it was discovered
2 late in the process.

3 I ask you to consider being the
4 champion for accelerating and getting a DOE
5 policy/directive/manual/whatever it takes to
6 give Contract a head start on what they are
7 really going to have to do about this.4

8 DR. TRIAY: As you know, we work
9 very closely with HSS [Health, Safety, and
10 Security]. Mr. Glenn Podonsky is a tireless
11 worker when it comes to addressing issues of
12 this nature. In order to establish the 2009-1
13 implementation plan we have established in the
14 Department a risk working group. The QRA has
15 been fully vetted with the risk working group.

16 The independent peer review that the
17 risk working group charter on the QRA has
18 given findings and conclusions to the HPAV
19 Independent Review Team. The Secretary has
20 stated in the implementation plan for
21 Recommendation 2009-1 that when the Department
22 used quantitative methods to inform safety

1 analysis it did so in a manner that was
2 consistent with accepted industry standards.

3 The Risk Working Group as a result
4 have sponsored the QRA peer review that I was
5 just referring to. I believe that the work of
6 the technical authority board will serve to
7 inform the ultimate addressing of
8 Recommendation 2009-1 just like we did with
9 the Standard 1189.

10 MEMBER MANSFIELD: I would just
11 counsel you that there is more to QRA than
12 Abelian algebra spreadsheets, etc., etc. It's
13 all in the models. It's all in what physics
14 you put into it and what uncertainty is in
15 there. That's what there needs to be a policy
16 on.

17 DR. TRIAY: As we have done before,
18 we will have a wide guidance on the subject of
19 the QRA and we will establish a pilot with NEM
20 like I was discussing yesterday that will
21 inform the work of the division.

22 I would also like to point out, Mr.

1 Mansfield, that very detailed level 3 PRAs are
2 used in the commercial nuclear world and those
3 analyses do not irrevocably lead to complex
4 controls. I believe that we will satisfy the
5 Board with respect to the QRA process.

6 We will establish clear guidelines
7 for this, as well as other programs in the
8 Department and in the Environmental Management
9 Program moving forward. I do believe that
10 this is going to be a very important tool in
11 the nuclear world within the Department of
12 Energy like it is already as a best industry
13 practice.

14 MEMBER MANSFIELD: I just wanted to
15 get that little lick in there.

16 Mr. Ashley, I want to quote
17 something from the 021 report on page A-3.
18 "The use of a relative probability among event
19 sequences calculated with an ignition
20 probability of one rather than an absolute
21 value, for instance, 10 to the minus 5 as a
22 threshold, will be less sensitive to model

1 uncertainties." Can you tell me what that
2 means?

3 MR. ASHLEY: What they means is if
4 you look at certainly the preliminary results
5 that we provided out of our quantitative risk
6 analysis, and I think they have affectionately
7 been referred to as the horse tails, it is
8 pretty clear that once a bubble forms that is
9 ignitable, that is combustible, the
10 probability of ignition then equal to one is
11 overriding in terms of that probability
12 distribution.

13 The comment is that as we go into
14 the sensitivity, as we develop the additional
15 probability distributions, the feeling, the
16 judgment is that may not significantly change
17 the outcome of the analysis based on that one
18 parameter which is not a distribution. It's
19 a probability of one of ignition.

20 As we go through the sensitivities
21 we may find as we go through those and
22 development of the design tool, we may find

1 that is an overriding parameter that drives
2 the results.

3 MEMBER MANSFIELD: Thank you. I
4 think I understand. On page A-5 in listing
5 the plant level events, you have process pipe
6 leaks and fires and floods and things. You
7 don't explicitly have loss of offsite power,
8 although it's mentioned at the bottom of A-4.
9 Are you going to consider loss of offsite
10 power in the distribution for repair time or
11 restoration time as initiating events?

12 MR. ASHLEY: Yes.

13 MEMBER MANSFIELD: And distribute
14 them?

15 MR. ASHLEY: Yes.

16 MEMBER MANSFIELD: Okay. Your
17 response to finding 2-6 I find particularly
18 heartening. You have committed yourself to
19 include -- you're going to update the design
20 tool to include distributed values in lieu of
21 point values in all other instances except
22 those where there is sparse data or not agreed

1 upon among subject matter experts and be
2 justified by industry experience. I think
3 that is very helpful.

4 I just urge you there are ways of
5 getting probability density functions when
6 data is sparse and not agreed to as well,
7 extreme value theory type thing. It's never
8 a good idea to leave tails out. If they are
9 going to hurt you in mono calculation, they
10 are going to hurt you anyway so you don't want
11 to eliminate it before you start.

12 MR. ASHLEY: Yes.

13 MEMBER MANSFIELD: Ms. Busche,
14 could you ever handle a safety analysis that
15 had a probability of ignition less than one?
16 Would you know what to do with it?

17 MS. BUSCHE: The answer is yes, I
18 could handle it. Right now with the current
19 design I have no mechanism to actually write
20 a meaningful control for that because I don't
21 know what I don't know. It's a pretty complex
22 design.

1 MEMBER MANSFIELD: It's complex
2 enough that everybody that I know that runs
3 into this problem controls it by having
4 ventilation and igniters which is what you had
5 in the original safety class design.

6 I've got a few things here. I'm
7 almost finished here. On page A-10 you talked
8 about a common relationship between the
9 normalized run-up distance, cell size, and
10 reaction zone length. Dr. Shepherd, can you
11 tell me is this something new that I haven't
12 heard of?

13 DR. SHEPHERD: This is a pretty
14 arcane bit of physics but I guess we can talk
15 about it. The situation we're talking about
16 is we've got a section of pipe which is
17 partially or totally filled with combustible
18 gas. We're imagining we have a small ignition
19 source at one end so we start with a flame.

20 Through the process of flame
21 instability and generation of turbulence that
22 flame accelerates and ultimately becomes a

1 detonation. The distance that it requires for
2 that to take place, that's the run-up length.

3 The question is we would like to be
4 able to predict that because clearly if things
5 don't transition to detonation, then
6 detonation is not something we need to be
7 considering in the safety analysis for that
8 particular situation. We need to have some
9 type of a correlation because this is not
10 something that is simple to predict.

11 It involves turbulence, one of the
12 last unsolved problems in classical physics.
13 It's quite complex so we resort to doing
14 experiments. The question is what would you
15 correlate that with. What do we have in terms
16 of dimensions.

17 We'll do a little dimensional
18 analysis here in class so we can have the
19 diameter of the pipe. We can have some
20 characteristic measure of the chemical
21 reaction length in the material. That's what
22 this cell size is about. You take those three

1 things and obviously there needs to be some
2 functional relationship.

3 You have to do a little bit of
4 thinking about that. There are some
5 scientists who have worked in this area and
6 they have thought about how that might work
7 and that's what this is all about.

8 MEMBER MANSFIELD: It's much more
9 clear when you describe it than it was on page
10 10.

11 DR. SHEPHERD: Yes.

12 MEMBER MANSFIELD: On page 11, I
13 believe you're saying that you're going to
14 generate distributed hydrogen generation rates
15 -- will be developed. My question is when.
16 Is there a program to come up with a PDF,
17 probability density function, for gas
18 generation rates?

19 MR. ASHLEY: Yes. That's one of the
20 variables that previously was input as a point
21 variable where we are in the process of
22 generating probability distribution.

1 Dr. Mansfield, a couple of things
2 that I need to clarify for the record. I
3 think you probably just misspoke but the
4 previous design did not have igniters in the
5 WTP.

6 MEMBER MANSFIELD: Well, you
7 potentially have mason iron and silver and
8 waste. Those are --

9 DR. SHEPHERD: But the implemented
10 control did not have igniters. We did have
11 vents.

12 MEMBER MANSFIELD: You had purges.

13 DR. SHEPHERD: Purges and flushes
14 but didn't have igniters.

15 MEMBER MANSFIELD: No, no. You
16 don't. I should say there are ignition
17 sources in that waste. It would be very hard
18 for anybody to try to convince you that the
19 waste mixture didn't have any nascent metals.

20 MS. BUSCHE: That is correct.

21 MR. ASHLEY: The other thing that I
22 did misspeak earlier, the only WAC [Waste

1 Acceptance Criteria] requirement is a
2 measurement of hydrogen. There are no other
3 gases that are required to be measured in the
4 WAC.

5 MEMBER MANSFIELD: So you're just
6 going to assume that there's enough -- there
7 are issues where -- I can think of batches
8 where you would have very depleted nitrates
9 and I don't --

10 MR. ASHLEY: We assume the oxidant.
11 We assume the oxidant in the proportions so
12 what we're interested in is the explosive gas,
13 the hydrogen. We've evaluated that's the
14 controlling mixture against the other gases,
15 the methane.

16 MEMBER MANSFIELD: But then the
17 nitrogen and the rest of the oxidant are
18 diluting gases.

19 MR. ASHLEY: Yes. That's one of the
20 HPAV independent review team findings that we
21 have to address. As I said, those other gases
22 cause a larger gas bubble which could change

1 the dynamics.

2 MEMBER MANSFIELD: There were two
3 areas in here where it was uncertain enough to
4 me that I have to ask the question. This is
5 do with finding 4-2. Is the ignition location
6 distributed? The ignition source location.

7 MR. ASHLEY: The ignition source is
8 assumed to be where the bubble occurs.

9 MEMBER MANSFIELD: Okay. It's in
10 the worst spot in the bubble.

11 MR. ASHLEY: We actually -- the
12 location at which it starts is stochastic. I
13 think Dr. Shepherd can better speak to that
14 but it is stochastic. It could occur anywhere
15 in the bubble.

16 MEMBER MANSFIELD: Okay. It won't
17 be at the worst possible spot at one end to
18 give you maximum run-up or anything like that.
19 It's going to be stochastically determined by
20 whatever the bubble link has to be. We'll
21 skip that, too.

22 I'm coming rapidly to the end and I

1 just want to ask Dr. Shepherd when the long-
2 awaited tests on axial pulsing loading are
3 going to be completed. Weren't you tasked by
4 DOE to do some tests of axial loading?

5 DR. SHEPHERD: I'm a little
6 mystified, Dr. Mansfield. What are you
7 referring to precisely?

8 MEMBER MANSFIELD: I'm quoting from
9 one of the thousands of pages of paper that
10 Mr. Ashley gave me but I won't trouble you
11 with this here. My last question is really an
12 observation. I think it's a healthy rule in
13 Monte Carlo calculations to run them uselessly
14 long until you get a few outliers to
15 understand what the world is really doing.
16 You don't have to do that for every situation
17 but I know people that have been caught
18 because they haven't done that.

19 All right, Mr. Chairman.

20 CHAIRMAN WINOKUR: Thank you, Dr.
21 Mansfield.

22 Mr. Bader.

1 MEMBER BADER: Before I start on
2 the mainline of the questioning, I wanted to
3 follow up on the QRA. I had a question for
4 Dr. Triay. I'm looking at the peer review
5 that was done of the QRA methodologies and one
6 of the concluding sentences says, "Without
7 further refinement of the modeling and
8 treatment of uncertainty the WTP runs the risk
9 of making inappropriate design decisions." I
10 don't think that's anything you can let stand
11 or anybody would want to leave standing.
12 Could you address how that's being resolved,
13 please?

14 DR. TRIAY: Yes. The HPAV
15 Independent Review Team took all of the
16 comments from the Risk Working Group sponsor,
17 a peer review team, and have given us very
18 specific recommendations and paths forward
19 which we do intend to implement. As I have
20 testified, until the HPAV Independent Review
21 Team looks at how we are intending to close
22 their issues, we're not pressing forward with

1 a finalizing the changes in the design.

2 MEMBER BADER: Is this something
3 that you would like to submit some additional
4 material on later?

5 DR. TRIAY: We would be happy to
6 submit for the record the statement of Dr.
7 Krahn as well as a detailed explanation of how
8 we are going to close the recommendations of
9 the Independent Review Team.

10 MEMBER BADER: Thank you.

11 Ms. Busche, we are going to repeat
12 some things, I think, that we touched on
13 yesterday in the evening. I believe you
14 agreed that the QRA design approach is a
15 qualified safety basis tool, or is not yet a
16 qualified safety basis tool. Is that correct?

17 MS. BUSCHE: Yes. Its primary
18 purpose is a design tool and it is not -- I'm
19 a little hesitant of the word qualified. The
20 use and application of that design tool is not
21 clearly established.

22 MEMBER BADER: Yes. It must meet

1 NQA-1 requirements under 414-1C.

2 MS. BUSCHE: Oh, yes.

3 MEMBER BADER: It has to be V&V.

4 Is that correct?

5 MS. BUSCHE: Correct.

6 MEMBER BADER: Going from there I
7 think we have discussed adequately the need to
8 protect certain assumptions which you will
9 have to determine as your analysis goes on.

10 MS. BUSCHE: Correct.

11 MEMBER BADER: And also calculated
12 results.

13 MS. BUSCHE: Correct.

14 MEMBER BADER: I believe we also
15 touched on whether or not you currently had
16 enough information to do a plan to write the
17 TSRs and LCOs [Limiting Condition of
18 Operation] and I believe your answer was no
19 you don't.

20 MS. BUSCHE: It's across the board.
21 Yes, correct.

22 MEMBER BADER: I really have only

1 one major area of concern that we haven't
2 addressed that comes out of all these things.
3 I've been making a short list. We have as yet
4 to be done large-scale testing, resolution of
5 the HIRT findings, and then use of the QRA as
6 a design tool, again a first-of-a-kind
7 application.

8 Mr. Ashley, my understanding is that
9 you are considering that the design is not
10 complete until the safety basis is completed.
11 Is that correct? In other words, you may find
12 things as a result of developing the safety
13 basis that impact your design.

14 MR. ASHLEY: The design criteria has
15 been established. We obviously have to
16 complete the development of the probability
17 distribution and the VNV of the quantitative
18 risk analysis we need to complete the
19 calculations necessary to support the
20 methodology. We have a schedule for
21 completing that.

22 The criterion methodology at that

1 time will be complete for implementation.
2 Now, the process of implementation, running
3 the QRAs for each of the individual routes,
4 running the piping analysis, along with
5 completing the design is going to be the
6 purchase of components that are qualified.
7 That is a process.

8 What Ms. Busche is referring to are
9 there going to be any additional inputs and
10 assumptions used in the QRA that will then
11 have to be protected as part of the safety
12 basis of the facility.

13 MEMBER BADER: I'm not being clear.
14 As a result of the large-scale testing as a
15 result of implementing the HIRT findings and
16 what comes out of the analysis of these
17 findings, to me there is a real risk that you
18 may find something that challenges a piece of
19 your design and has to be incorporated.

20 MR. ASHLEY: Understand the design -
21 - the changes in the design are not complete
22 or they have not been started. I need to

1 clarify there is no additional planned large-
2 scale testing. These is component
3 qualification testing.

4 MEMBER BADER: No, no. I'm going
5 back to mixing.

6 MR. ASHLEY: Oh.

7 MEMBER BADER: I'm sorry. I'm not
8 being clear enough. I'm looking at the whole
9 project now and looking at the number of
10 things that have to be addressed so large-
11 scale testing of the pulse jet mixing. Then
12 the HIRT findings have to be implemented, have
13 to be addressed and the fixes implemented.

14 To me all these things you're going
15 to find something in all of this that impacts
16 your design. It's going to have to be
17 reflected in Ms. Busche's safety analyses and
18 work. Then your design is going to be
19 impacted by what she finds. Is that correct?

20 MR. ASHLEY: Yes. That process
21 between design and nuclear safety is an
22 iterative process. Any design change is

1 reviewed by nuclear safety to determine if
2 we've introduced additional hazard. If we've
3 introduced additional hazard, that has a
4 potential iterative affect on design. That is
5 the design process in the nuclear industry.

6 MEMBER BADER: What this takes me
7 to is the concern that there will be pressure
8 on your, Ms. Busche, to do your work. I think
9 the pressure is going to come from unexpected
10 sources. I mean, there is a real desire to
11 finish this plant to get it up and running.
12 Do you feel up to this working under this kind
13 of pressure?

14 MS. BUSCHE: Yes.

15 MEMBER BADER: And that takes me
16 really to my last question which is, Mr.
17 Russo, I hope you are going to support Ms.
18 Busche in what she needs to do and do it
19 unequivocally, directly, and simply and that
20 you are going to protect her.

21 MR. RUSSO: I think she will tell
22 you that about seven months ago I met her

1 outside of a meeting where there was that
2 healthy tension between design and safety
3 basis. I said, "Donna, I have your back."

4 MS. BUSCHE: That was a true story.

5 MEMBER BADER: I expect Mr. Knutson
6 and Dr. Triay would support Mr. Russo in that.

7 MR. KNUTSON: Absolutely. Donna is
8 an incredibly talented talent and incredibly
9 important part of the project team.

10 DR. TRIAY: As you know we have a
11 network of nuclear safety experts with the
12 Environmental Management Program that work
13 very closely together. Their leader is the
14 Deputy Assistant Secretary for Safety and
15 Operations Oversight. Our complete support is
16 always given to that network of nuclear safety
17 experts because of their excellent work have
18 led to the Department having very robust
19 nuclear safety record.

20 MR. SAIN: I would like to add that
21 URS supports Donna fully with the stable of
22 safety basis experts that we've got.

1 MEMBER BADER: Those are the
2 answers I fully expected I would get but I
3 wanted to ask to be sure. I'll ask Ms. Busche
4 one final question and that is are you ready
5 for the opportunity on a plant that's got a
6 lot of first-of-a-kind things to have the
7 first-of-a-kind safety basis for QRA?

8 MS. BUSCHE: Yes.

9 MEMBER BADER: I have no further
10 questions, Mr. Chairman.

11 CHAIRMAN WINOKUR: Mr. Dwyer.

12 MR. DWYER: Just for clarification.
13 Dr. Shepherd, in your response to question 12
14 that the Board received from DOE --

15 DR. SHEPHERD: Yes.

16 MR. DWYER: -- you indicated that
17 you were not yet satisfied with, I guess, the
18 resolution of some issues you raised with
19 Dominion Engineering. Has there been any
20 further development?

21 DR. SHEPHERD: Thanks for the
22 opportunity. This goes to the question that

1 Ms. Roberson asked me at the beginning of the
2 session. I have gone back and I've looked at
3 the correspondence. I would like to say in
4 general that I have been very satisfied with
5 the responsiveness of both Bechtel and
6 Dominion to my comments.

7 It often takes some time due to the
8 complexity not only of the technical issues
9 but the contracting to get those resolved. I
10 have a long-term commitment to this project.
11 I'm tenacious in getting my concerns
12 addressed. There are some folks here in the
13 audience who can attest to that.

14 In this particular case for this
15 particular letter that I wrote on March 27th
16 there were four documents that I reviewed. I
17 have had discussions with Dominion staff and
18 Bechtel about those. We have discussed a path
19 forward that I believe will resolve my issues.

20 I think that they have been
21 otherwise occupied in the last six months and
22 have not gotten back to that but I have spoken

1 with Craig Jones and Mike Wintick about it and
2 there is a plan to have those addressed. I
3 expect to be reviewing those documents this
4 fall.

5 MR. DWYER: So the summary is you
6 believe you have a path forward but resolution
7 not yet achieved?

8 DR. SHEPHERD: Yes. That's right.
9 I don't see any obstacles to resolving that.
10 It's a matter of their returning a draft to
11 me, my going through that discussing it with
12 them resolving any remaining issues. That's
13 typically the fashion in which this gets done.

14 MR. DWYER: That's all.

15 MEMBER BADER: Dave, did you want
16 to make a comment?

17 MR. BROCKMAN: Yes. I just wanted
18 to add to your concern that you posed to Ms.
19 Busche. The authorization basis approval and
20 the oversight of that and watching that is,
21 you know, independent in my office. I can
22 assure you we watch for that very closely and

1 won't allow it.

2 MEMBER BADER: Thank you.

3 CHAIRMAN WINOKUR: I have a few
4 questions. In the answers to the questions
5 you talked about, I guess you used the words
6 "readily accomplish repair" if there is a
7 breach in piping in the hot cells. Can you
8 give some insight into what that will involve
9 and the time frames and depending on the kind
10 of waste it is whether it's a slurry or some
11 other type of waste.

12 MR. ASHLEY: To begin with, you
13 know, I think it warrants addressing for the
14 record some of the statements about the
15 consequences and how catastrophic the
16 consequences may be. I think it is important
17 once again to reiterate that the piping is
18 designed -- the piping and inline components
19 will be designed to withstand these events.

20 Now, if you go to the extreme that
21 the probabilities are never zero and if there
22 were damage to a piping component that was in

1 the hot cell, the expectation is that damage
2 would result in a leak. Many of these
3 components are not welded components, the
4 jumpers. They are made to be replaceable.
5 That equipment has to be removable for repair
6 and maintenance.

7 The expectation is that a repair or
8 replacement would be similar to a repair or
9 replacement necessary for normal plant
10 maintenance. Part of our OR model is
11 evaluating how long it takes if we have a pump
12 failure, if we have a valve failure under any
13 situation.

14 It could be just normal failure,
15 wear failure, any other type of failure
16 operations has looked at, what it would take
17 under those normal service conditions to
18 replace those components. The expectation is
19 the causes of damage due to -- potential cause
20 of damage due to a hydrogen event would be
21 very similar.

22 CHAIRMAN WINOKUR: Does that include

1 the cleanup of the waste? How does that
2 factor in in terms of what it would take to
3 become operational again in that area.

4 MR. ASHLEY: I don't believe
5 operations has developed all of the procedures
6 necessary. There will be leaks in the cell.
7 Jumpers will leak over the life of the
8 facility. The cells are lined. The cells
9 have sumps so they are designed to facilitate
10 any necessary cleanup if there were a spill or
11 a leak in the cell.

12 CHAIRMAN WINOKUR: Let's assume
13 there was this leak or this serious leak. How
14 long would it take to clean it up? What do
15 you think?

16 MR. ASHLEY: I don't have that
17 information. We can provide that for the
18 record. I would need to consult with the
19 operations folks.

20 CHAIRMAN WINOKUR: All right. I've
21 gotten so few notes during this hearing but I
22 did get one so I have a question for you, Dr.

1 Shepherd. Obviously there was work done in
2 Southwest Research Institute and they
3 developed the pressure time histories. Do you
4 have any concerns about the studies that they
5 performed whether they were valid or not?

6 DR. SHEPHERD: I believe their work
7 is valid. I think there are particular
8 details that we've discussed that need careful
9 attention to but by and large it's valid.

10 CHAIRMAN WINOKUR: Okay. My final
11 question is for you, Mr. Knutson. We barely
12 met. We just heard throughout these
13 discussions this morning that this design is
14 not complete at this point so the question is
15 how does DOE pivot the project when the design
16 is not complete? What does that mean?

17 MR. KNUTSON: I think I talked about
18 that a little bit yesterday. We've spent a
19 lot of time talking about the pre-treat
20 facility. There are five facilities in this
21 project. The pre-treat facility is the one
22 that we are reserving the most open schedule

1 time to be able to respond to issues that may
2 emerge from testing or QRA responses or even
3 the development of the TSRs.

4 It's a very large project and there
5 is an awful lot of that project that needs to
6 be moving towards commissioning and start-up
7 and that's what I mean by saying it's time to
8 pivot.

9 There may be elements of the project
10 that we need to take in all deliberate haste
11 and ensure ourselves that the path forward is
12 clear and within the expectations that we've
13 set for performance on this project. That
14 doesn't mean the rest of the project needs to
15 stand still waiting for that.

16 CHAIRMAN WINOKUR: So the pivoting
17 doesn't mean that you don't have a design
18 effort going on still?

19 MR. KNUTSON: That's correct.

20 CHAIRMAN WINOKUR: Okay. Dr. Triay,
21 is there anything you want to say about that?

22 DR. TRIAY: I completely agree with

1 what Mr. Knutson has said. We designed the
2 concept of trying to ensure that the rest of
3 the program was ready to feed the waste to the
4 waste treatment plant, that the rest of the
5 infrastructure was ready.

6 As a matter of fact, we assigned
7 \$300 million of Recovery Act monies to the
8 tank farm infrastructure so that we could be
9 ready for the commissioning and ultimate
10 operations of the waste treatment plant. I
11 believe that Mr. Knutson is correct that this
12 is the appropriate time for that transition in
13 the site office.

14 I believe that Mr. Brockman is of
15 the same opinion. We will work very closely
16 together to ensure that when this plant starts
17 operating the rest of the infrastructure is
18 ready to support its safe operations.

19 CHAIRMAN WINOKUR: Thank you. Do
20 other Board members have questions?

21 VICE CHAIR ROBERSON: No.

22 CHAIRMAN WINOKUR: All right. I

1 want to thank our witnesses very much. This
2 concludes the testimony from our staff as well
3 as the Department and its contractors and
4 their experts.

5 We will now call on members of the
6 public who have signed up to speak. As I
7 indicated earlier, I ask that each speaker
8 limit remarks to about five minutes. If time
9 permits, I will extend that time for
10 additional comments.

11 The first person on the speaker list
12 is Jen Gregory.

13 MS. GREGORY: Hello. I want to
14 thank you for this opportunity to present
15 public comments. My name is Jen Gregory and
16 I work for Hanford Challenge, an organization
17 that works in the public interest for a safe
18 and robust cleanup at Hanford.

19 You know, I think public comments
20 are particularly important when making
21 assessments about actions that could result in
22 increased risks. Deciding the safety

1 tradeoffs for time, money, or other reasons is
2 essentially a value judgement. I am hear
3 today to say that as a member of the public I
4 value erring on the side of safety.

5 To that end, I want to continue
6 presenting Hanford Challenge questions that
7 were interrupted yesterday. Why is a design
8 that cannot prevent flammable gas explosions
9 considered acceptable? There is a design
10 solution that prevents these explosions but it
11 is considered too expensive. Are explosions
12 in a hazardous nuclear facility ever
13 acceptable?

14 Why is a possibility of a nuclear
15 criticality considered acceptable at the waste
16 treatment plants? Internal documentation
17 indicates that nuclear criticality could occur
18 if the waste tanks are not adequately mixed
19 and plutonium settles to the bottom of the
20 tank.

21 Why has Bechtel proposed redefining
22 firewalls in the facility as non-safety items

1 to save on cost? What justification can there
2 be besides money to propose such a move? Is
3 DOE considering the implications a broken
4 safety culture has on the safety of a waste
5 treatment plant? How will concerns surface if
6 employees who notice critical issues are
7 afraid to raise their concerns?

8 Why did DOE suddenly approve the
9 closure of technical issues after their own
10 work plans concluded that it will take 18
11 months or more to resolve these issues? Is
12 this approval related to the fact that the DOE
13 had a legally binding tri-party agreement
14 cleanup milestone to meet and that Bechtel had
15 \$6 million at risk if they didn't close a key
16 technical issue M3 by June 30th?

17 Is DOE considering the impact of
18 assigning one contractor to design and build
19 the waste treatment plant and another
20 contractor to operate the plant? Since
21 Bechtel is not responsible for operating the
22 plant, there is no contractual penalty if they

1 build a plant that does not work.

2 For the first six years of design
3 and construction of the waste treatment plant
4 Bechtel lacked a vendor quality assurance
5 program. How can we assure that the quality
6 of procured equipment and instruments is
7 adequate without the necessary pedigree?

8 Would this facility even be
9 considered for licensing by the Nuclear
10 Regulatory Commission or denied due to its
11 quality indeterminate state? Doesn't the
12 public deserve a plant that meets the safety
13 standards of an NRC licensed facility?

14 When the atmosphere has been
15 poisoned by a history of reprisals against
16 employees who raise concerns, the quality and
17 safety of the plant will always remain
18 indeterminate because important issues
19 affecting future operations may not have been
20 raised and addressed.

21 The waste treatment plant design,
22 especially the strategy of pre-treatment of

1 the waste, is in jeopardy of failure. Meeting
2 deadlines to build a plant have overridden
3 safety and design considerations for the
4 operation phase. Thank you.

5 CHAIRMAN WINOKUR: Thank you, Ms.
6 Gregory. Please submit those comments for the
7 record.

8 The next speaker is Liz Madsen.

9 MS. MADSEN: Thank you for
10 soliciting comments from the public on the
11 issues that surround the design and
12 construction of Hanford's waste treatment
13 plant. My name is Liz Madsen and I work for
14 Hanford Challenge. I am also the Vice Chair
15 of the Public Involvement Committee of the
16 Hanford Advisory Board.

17 I appreciate your effort to bring
18 issues into the light and clarify the
19 confusion that surrounds this much-delayed
20 project. I am going to use the pronoun "we"
21 today.

22 I believe in systems that hold us

1 accountable and believe that in the end as we
2 age and die and the problems of Hanford go on,
3 we all take some responsibility in our
4 individual roles for shifting and changing and
5 finding the best solutions to achieve a robust
6 and complete cleanup.

7 A cornerstone of that cleanup is the
8 waste treatment plant. Hanford brings with it
9 incredible uncertainties. We have some
10 records. We have some sampling data but often
11 it is not enough information for actions and
12 assessments that require a high degree of
13 certainty.

14 Of importance to the waste treatment
15 plant is our lack of knowledge about Hanford
16 tank waste. Over the past few years I have
17 seen over and over how a situation with high
18 degrees of uncertainty results in pretending
19 that everything is under control and a default
20 position that when in doubt nothing is wrong.

21 As a member of the public I
22 appreciate any effort to cultivate an

1 environment of transparency and openness where
2 expressing what we don't know is encouraged so
3 that we can get to a place of knowing.

4 Posturing confidence and knowledge wastes
5 precious time and tends to take us further
6 from robust solutions.

7 Yesterday a member of the DNFSB
8 showed a pointed observation from the
9 discussion defining how an issue can be closed
10 when it is unresolved. What is closed is not
11 closed. I wish it was not such a challenge to
12 use clear language and say what we mean. I
13 wish that profit and schedule were not such
14 seductive factors in a game to make the right
15 decision.

16 I am tired of seeing and hearing
17 about plans for solutions that are not
18 believable. I often think about the time
19 frame of Hanford cleanup and long-term
20 stewardship. When I look around this room I
21 wonder who will still be working on this
22 project in 10 years, 20 years? Where is the

1 dedication to follow through and bring this
2 painful process to fruition?

3 As one of the rare young people
4 involved, it is disheartening to receive the
5 message that everything is going to be fine
6 and see so much evidence to the contrary.
7 After 10 years no one in this room can
8 honestly assure me that the waste treatment
9 plant will operate safety and effectively.

10 Thankfully we are here in front of
11 the DNFSB in an effort to publicly bring in
12 some sunshine clarifying positions and finding
13 truth in a situation that is so mired in
14 complexity and confusion.

15 It is my hope that everyone involved
16 is reminded frequently of the bigger picture.
17 We are here to protect future generations. I
18 want to tell my grandchildren a story that
19 ends, "Despite all the problems that plagued
20 Hanford, we worked together and successfully
21 designed a plant that secured extremely
22 dangerous waste in glass to protect you."

1 Thank you.

2 CHAIRMAN WINOKUR: Thank you, Ms.
3 Madsen. Please submit that for the record.

4 I may pronounce this name wrong.
5 John Stang.

6 MR. STANG: That is correct.

7 CHAIRMAN WINOKUR: It's not your
8 name that's difficult. It's the handwriting.

9 MR. STANG: That's probably true.
10 I'm a reporter from Seattle. I don't have any
11 comments but I'm here to ask two questions of
12 Mr. Bader if I may.

13 CHAIRMAN WINOKUR: No, I don't
14 believe we are going to entertain questions at
15 this point.

16 MR. STANG: Okay. I was told
17 yesterday that this was the appropriate way to
18 ask questions.

19 CHAIRMAN WINOKUR: No, I don't
20 believe so. You'll have to put them on the
21 record and we'll answer them. This is an
22 informational meeting. The Board will not be

1 taking questions.

2 MR. STANG: Okay. I don't
3 understand.

4 CHAIRMAN WINOKUR: I'm sorry for the
5 misunderstanding. Please just submit them for
6 the record. We will get back to you.

7 MR. STANG: In writing?

8 CHAIRMAN WINOKUR: Yes.

9 MR. STANG: Okay.

10 CHAIRMAN WINOKUR: Thank you.

11 There are two more names on this
12 list here and I have to just as a matter of
13 protocol make sure that they are not present
14 now, or wish to speak, that is. Susan Lekband
15 and Allen Bolt. My apologies. There was a
16 second page. Dick Dunning.

17 MR. DUNNING: Good morning, Mr.
18 Chair. It's actually Dirk Dunning. Today I'm
19 speaking entirely on behalf of myself. I'm a
20 registered professional chemical engineer also
21 trained in nuclear environmental control
22 systems and several other fields of

1 engineering.

2 I just wanted to make a couple of
3 points. First I'll start by thanking you all,
4 the Board and the staff, for your diligent
5 work on all of this subject and all of the
6 long hours I know that you've put in by the
7 questions that you've asked. It's greatly
8 appreciated.

9 I also want to thank you very much
10 for your openness and transparencies in this
11 entire process. It's greatly appreciated by
12 all the citizens of the Northwest.

13 I would also echo Liz Madsen's final
14 closing comment that though there are problems
15 in building a facility of this complexity, and
16 there will be more, and some of them will be
17 really hoary, solving them is essential to
18 getting this plant operating and getting this
19 plant operating is essential for the
20 Northwest. Whatever these problems are we
21 need to find them and we need to resolve them.
22 All of the help of everyone involved is

1 essential in doing that.

2 In listening to the discussions
3 there are a couple of points that I think
4 could use some clarification. Back about 15
5 years ago or more as the Hanford tanks were
6 going through what were called rollover events
7 as gas was generated and the tanks would roll
8 over the researchers involved calculated that
9 the potential ignition energy was seven
10 millijoules for those gases.

11 That's extremely low. As you're
12 talking through the probabilities of ignition
13 and whether it should be one or something
14 else, with those kinds of energies I don't
15 doubt that there is the potential for ignition
16 wherever it is and that we don't know what
17 that is.

18 Something else for people who are
19 not from this region, and even for those here.
20 Hanford and the Northwest is home to the
21 Cascadia fault system off the
22 Oregon/Washington coastline. This is a fault

1 that is 1,000 kilometers long, about 100 miles
2 offshore. About every 350 to 1,100 years it
3 ruptures.

4 When it does that it ruptures with a
5 9.5 earthquake that goes on for about five-
6 and-a-half minutes. The expectation from the
7 studies is that if that event occurs at some
8 time in the next 50 years, all of the bridges
9 in western Washington and Oregon will
10 collapse.

11 Transportation systems will be down.
12 The major fuel transports out of Anacortis
13 heading south through Washington state into
14 Oregon will be disrupted for months at a time.
15 There isn't going to be any easy recovery and
16 there isn't going to be anybody coming to help
17 in the real near term. We are all going to be
18 on our own wherever we are in the region so I
19 would be very careful about that.

20 Also, it's important in recognizing
21 that those events principally people think
22 about earthquakes as having the first two

1 modes, the shear and compression waves, the P
2 and the S waves. What is often forgotten is
3 there are two other modes, the Love and
4 Rayleigh waves.

5 Particularly in large subduction
6 zone events the Love waves are important.
7 Those waves are at lower frequency roughly
8 with wave lengths comparable to the size of
9 the facilities and vessels at Hanford. Those
10 can cause somewhat different kind of
11 responses. It changes the spectral response
12 frequency and that's important in the
13 analysis.

14 Those are the principal ones I just
15 wanted to make sure you guys were aware of.
16 Again, thank you for all of your diligent
17 effort and work and keep it up.

18 CHAIRMAN WINOKUR: Thank you, Mr.
19 Dunning.

20 Larry Felton. Mr. Felton. Mr.
21 Felton is not present.

22 That concludes the public comment

1 portion of this hearing. I would now like to
2 turn to the Board members to see if they have
3 any closing comments.

4 MEMBER BROWN: No.

5 VICE CHAIR ROBERSON: No.

6 MEMBER MANSFIELD: No.

7 MEMBER BADER: No.

8 CHAIRMAN WINOKUR: I'm going to
9 provide some very general closing comments and
10 then I will close the meeting.

11 This public meeting and hearing
12 dealt with public health and worker safety for
13 the waste treatment plant at Hanford which is
14 DOE's solution to cleaning up the toxic and
15 radioactive waste in Hanford's tank farms.

16 The first session looked at the
17 adequacy of pulse jet mixer vessels and
18 implications for the waste acceptance
19 criteria, the Board's safety concerns or
20 criticality, hydrogen gas buildup, and PJM
21 mixer overblows. The Board was pleased the
22 Department has committed to accelerate large-

1 scale testing of pulse jet mixer vessels
2 beginning in 2012.

3 The Board also believes a hot pilot
4 plan during plant operation also has high
5 value.

6 During the second session on pre-
7 treatment facility safety. The Board explored
8 issues of complexity that drove a revised
9 hydrogen strategy and its implications on the
10 safety basis. The Board has always been
11 supportive of more reduction but has concerns
12 about severity level calculations dealing with
13 sprays and leaks and deposition velocity.

14 The Board is concerned that the
15 Department has chosen not to adopt a
16 deposition velocity of 0.1 to 0.3 that the
17 Department agrees is technically justified.
18 The Board is concerned that the requirements
19 on the tank farms to control, characterize,
20 and deliver waste to the waste treatment plant
21 will become increasingly complex if the waste
22 treatment plant is required to tighten its

1 waste acceptance criteria as it finalizes its
2 design.

3 Today's final session of this public
4 meeting and hearing explored the Department's
5 hydrogen strategy for pipes and auxiliary
6 vessels that employs a quantitative risk
7 assessment methodology.

8 The Board is concerned that the QRA
9 methodology may reduce the plant's margin of
10 safety resulting from breaches in the primary
11 confinement boundary in the hot cells which
12 may require repairs that delay operations and
13 expose workers to hazardous situations. The
14 Board would like to thank all of the witnesses
15 from the Department of Energy, its contractor
16 organizations, and its technical experts who
17 testified during these two days of public
18 meetings and hearings.

19 I want to personally once again
20 thank Dr. Triay. I want to thank all the
21 folks at DOE and their team. I thought this
22 was an excellent information exchange.

1 Obviously it's a very extensive record to
2 review and I appreciate you all being here.

3 With that I am going to close this
4 public meeting. The record of this meeting
5 will be open until November 7, 2010. Thank
6 you for coming.

7 (Whereupon, at 12:05 p.m. the
8 hearing and meeting were adjourned.)

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